

Fluid viscoelasticity affects ultrasound force field-induced particle transport

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(Received 25 March 2024; revised 30 July 2024; accepted 3 October 2024)

Ultrasonic standing wave technology offers an ideal platform for manipulating particles in microfluidics. We study how fluid viscoelasticity and acoustic boundary formation in micro-confinements affect ultrasound-induced perturbations. These perturbations influence acoustic energy density (AED) and consequently particle transport dynamics. Our approach combines theoretical, numerical and experimental methods. Using the Oldroyd-B model for viscoelastic fluids, we advance acoustic radiation force (ARF) formulations of Doinikov *et al.* (*Phys. Rev. E*, vol. 104, no. 6, 2021*a*; *Phys. Rev. E*, vol. 104, no. 6, 2021*b*) for particles much smaller than the acoustic wavelength. This improved approach allows us to decouple AED and acoustic contrast factor terms in the ARF expression. It also enables us to examine the effects of viscoelastic parameters: μ^* (ratio of the viscosity of the viscoelastic fluid to that of base Newtonian fluid) and De (product of fluid relaxation time and actuation frequency) on AED and particle migration. Remarkably, we show that increasing fluid elasticity or De transitions viscoelastic fluids from the energy dissipation (relaxation) mode to the energy storage (frozen) mode, increasing AED. Conversely, increasing viscosity (μ^*) reduces AED. Thus, our findings suggest that elastic effects accelerate particle migration, while viscous effects decelerate it. Consequently, a viscoelastic fluid-filled micro-confinement acts as an energy dissipation device at low De and an energy storage device at high De . Particle migration can be controlled by adjusting viscoelastic and acoustic parameters, at a fixed power input. Our theoretical and numerical findings are validated with our experimental data. Our study advances the fundamental understanding of particle migration in viscoelastic fluids under ultrasound, and can significantly impact future studies on particle/cell migration in bio-fluids.

Key words: microscale transport, viscoelasticity, shear waves

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1. Introduction

The manipulation of particles and cells in Newtonian and non-Newtonian fluids is crucial for biomedical and biochemical applications (Yuan *et al.* 2018). Various passive and active techniques have been used for particle and cell handling in microchannels (Sajeesh & Sen 2013). Recently, ultrasonic standing wave (USW) technology has gained attention for its contactless, gentle, biocompatible and non-invasive characteristics (Laurell, Petersson & Nilsson 2007). Exposure of particles to an ultrasound field results in nonlinear scattering, leading to time-averaged acoustic radiation force (ARF) (King 1934; Yosioka 1955; Lighthill 1978). In a Newtonian fluid, the primary ARF is proportional to particle volume (Bruus 2012*b*), acoustic energy density (AED) (Barnkob *et al.* 2010) and acoustic contrast factor (ACF) (Petersson *et al.* 2004), the latter being a function of compressibility of the particle relative to the suspending fluid and decides the direction of force. This dependency enables label-free manipulation of particles based on size, density and compressibility contrast (Bruus 2012*b*; Nath, Malik & Sen 2021; Malik *et al.* 2022).

Various theoretical and numerical studies have formulated ARF on small particles within the Rayleigh limit (Baasch & Dual 2018), for ideal fluids (Gorkov 1962; Bruus 2012*b*; Hoque, Nath & Sen 2021), viscous fluids (Doinikov 1997; Settnes & Bruus 2012) and thermo-viscous fluids (Karlsen & Bruus 2015), based on perturbation theory (Bruus 2012*a*) and first-order scattering theory (Settnes & Bruus 2012). The USW in the low MHz range generates a first-order pressure field with the pressure node and antinode within a microfluidic channel. For the fundamental resonance mode, i.e. a half-wave actuation, the node and antinode correspond to the channel centre and walls (Bruus 2012*a*), respectively. Particles suspended in a Newtonian fluid and exposed to ARF migrate to the node (positive ACF) or antinode (negative ACF) (Petersson *et al.* 2004). Barnkob *et al.* (2010) studied acoustic particle transport in such a fluid, traced particle trajectories over time and equated viscous drag with ARF to predict the AED. Experimental investigations on particle/cell migration (Laurell *et al.* 2007; Karthick *et al.* 2018; Nath *et al.* 2021) show that changes in fluid density, compressibility and viscosity affect AED and ACF, thereby influencing migration trajectory and migration time. This is important for ARF-driven separation and sorting of particles/cells in microchannels (Lenschof & Laurell 2010).

Owing to the rich property dependence of ARF, fluid viscoelasticity can significantly alter the ARF (Doinikov, Fankhauser & Dual 2021*b*). A viscoelastic fluid exhibits both viscous and elastic characteristics, enabling a time-dependent response to deformation, including stress relaxation and creep (Joseph 2013). Consequently, the motion of particles suspended in a viscoelastic fluid differs significantly from their motion in a Newtonian fluid. For instance, the first normal stress difference ($N_1 = \sigma_{xx} - \sigma_{yy}$), which is absent in Newtonian fluids, produces a viscoelastic lift force (Leshansky *et al.* 2007) on particles in viscoelastic fluids. Over the last decade, significant progress has been made in understanding particle migration and sorting enabled by fluid viscoelasticity (D'Avino, Greco & Maffettone 2017; Hazra *et al.* 2021). However, passive viscoelastic particle migration and sorting require a large shear rate and longer channel length. Additionally, passive sorting methods have disadvantages such as low separation efficiency and throughput (Yuan *et al.* 2018), which could be mitigated by exposing viscoelastic fluid systems to external force fields (Yuan *et al.* 2018).

Most microfluidic systems use complex bio-fluids such as blood (Lenschof & Laurell 2010), blood plasma (Brust *et al.* 2013), saliva (Stokes & Davies 2007), sputum (Li *et al.* 2016), synovial fluid (Rainer & Ribitsch 1985), protein solutions (Pan *et al.* 2009) or hydrogels (Chaudhuri *et al.* 2020). These bio-fluids possess complex rheology, with most being viscoelastic. For example, blood is a viscoelastic shear-thinning fluid due

to the dynamics, deformability, and interactions of red blood cells (Chien 1970; Brust *et al.* 2013). Studies on protein solutions (Pan *et al.* 2009), polymeric solutions (Rouse 1953), hydrogels and extracellular matrices (Chaudhuri *et al.* 2020) also highlight the significance of the viscoelastic nature of bio-fluids. Some of the existing studies have used ARF for manipulating particles suspended in bio-fluids in microchannels (Laurell *et al.* 2007; Lenshof & Laurell 2010). Even though these studies involve the use of complex bio-fluids, modelling and analysis of such systems often assume the fluid to be Newtonian. Since bio-fluids are inherently viscoelastic, the dynamics may not be captured well by treating the physics based on such simplified assumptions. Therefore, understanding the interaction of viscoelastic fluids with external acoustic fields in micro-confinements is of utmost importance to accurately decipher the physics. This could find relevance in better understanding particle transport characteristics, leading to important microfluidic applications (Sajeesh & Sen 2013; Yuan *et al.* 2018).

Although interaction between viscoelastic fluids and external force fields in a micro-confinement is yet to be understood, there are few reports which consider the effect of viscoelasticity on acoustic parameters. For instance, Hintermuller, Reichel & Jakoby (2017), Doinikov, Fankhauser & Dual (2021a) and Vargas *et al.* (2022), modelled Oldroyd-B and Maxwell fluids under ultrasound to study acoustic streaming. Recently, Doinikov *et al.* (2021b) theoretically formulated and numerically calculated the ARF on isotropic solid spherical particles in unbounded compressible viscoelastic fluids, without imposing any restriction on the particle size compared with the acoustic wavelength. They derived a generalized ARF expression using indefinite integrals, highlighting the complexity and precision required for these calculations. Their findings showed that boundary layer formation on particle surface and shear wave propagation affect wave scattering and ARF. However, their study focused only on the effects of the particle boundary layer on ARF. An understanding of the effects of boundary layers on the channel walls, shear wave propagation and viscous dissipation in the fluid on the incoming waves and ARF is missing in the literature. Furthermore, the decoupled effects of AED in the fluid and ACF on ARF and particle migration in viscoelastic fluids are yet to be investigated.

Recently, Vargas *et al.* (2022) examined the effects of viscosity and elasticity (Deborah number, De) on the perturbation field to study acoustic streaming, considering shear wave attenuation. However, their analysis is limited to extremely narrow microchannels where the channel depth (D) is comparable to the boundary layer thickness (δ_{ve}) but much smaller than the channel width (W) and acoustic wavelength (λ_0) ($\delta_{ve} \sim D \ll W \sim \lambda_0$). Due to the constraints in the perturbation method, they omitted higher-order viscous effects (assuming $\epsilon = D/\lambda_0 \ll 1$, neglecting second and higher orders of ϵ) and considered δ_{ve} only as a function of viscosity. Nonetheless, microfluidic devices used for particle manipulations often feature channel depth and width that are of the same order as the acoustic wavelength. In such cases, the solution provided by Vargas *et al.* (2022) becomes inadequate. Consequently, it is essential to advance the analysis for viscoelastic fluid cases where $\delta_{ve} < D \sim W \sim \lambda_0$ for microfluidic acoustophoresis applications. Further, there is no theoretical and experimental study reported, exploring acoustic particle migration in viscoelastic fluids inside a microchannel exposed to ultrasound, which serves the objective of the present study.

In summary, previous studies on particle dynamics in viscoelastic fluids exposed to ultrasound have mainly focused on acoustic streaming and the effect of the acoustic boundary layer near the particles on ARF. However, the impact of the boundary layer at the channel walls and viscoelasticity on the AED in the fluid, and consequently the ARF, has

not received attention. Further, there is a lack of understanding of the dynamics of acoustic particle transport in viscoelastic fluids inside a microchannel, specifically the decoupled effects of viscous and elastic effects. In this study, we investigate how fluid viscoelasticity and boundary layer formation along the channel walls influence acoustic perturbations in a fluidic channel having dimensions comparable to the acoustic wavelength, typical of a microfluidic acoustophoresis device. By considering the effects of boundary layers on the channel walls and adjusting the incoming acoustic field, we develop an improved formulation for the acoustic force in viscoelastic fluids inside a channel. This formulation decouples the effects of viscoelasticity on both the ACF and the AED. Further, through experiments and theoretical analysis, we explore the effects of viscoelasticity on acoustic particle migration dynamics in a microchannel. Our work addresses a significant gap in the literature, providing new insights into how viscoelastic properties impact acoustic migration phenomena.

In order to understand the sole effect of viscoelasticity on the ARF, neglecting any contribution from the viscoelastic lift force, we conduct the study in a quiescent fluid where the lift force vanishes. We use the Oldroyd-B model (Oldroyd 1950) to describe viscoelastic fluids as this model stands out for its simplicity and accuracy in capturing both viscous and elastic behaviours, making it ideal for representing the complex behaviours of bio-fluids and polymer solutions. We characterize viscous effects ($\mu = \mu_s + \mu_p$) via the viscosity ratio $\mu^* = \mu/\mu_{bf} = \mu_p^* + \mu_s^*$ and the elastic effects or fluid relaxation time τ via the Deborah number $De = \tau\omega$, where μ_p and μ_s are the polymer and solvent viscosities, μ is the total viscosity, μ_{bf} is the base Newtonian fluid viscosity and ω is the ultrasonic actuation frequency. In § 2, we introduce formulations for acoustic field perturbations in viscoelastic fluids, influenced by the acoustic boundary layer, which is a function of viscous and elastic properties. We develop a theory to determine the scattered acoustic field using first-order scattering theory with multipole expansion. We then derive a modified expression for the ARF by decoupling the AED and ACF and analyse particle migration dynamics. In § 3, we describe the numerical schemes for solving the perturbed governing equations and determining the AED. In § 4, we detail the experimental set-up and fluid properties. In § 5, we present and discuss the effects of μ_p^* , μ_s^* , De and acoustic boundary layer on the incoming field, AED, ACF, ARF and particle migration dynamics from theory and experiments using polyethylene oxide (PEO) and polyvinylpyrrolidone (PVP) solutions. Finally, conclusions are outlined in § 6.

2. Theoretical formulation

Exciting a fluid with sound waves under resonance condition induces fluid perturbations (Lighthill 1978; Bruus 2012a). Particles present in the fluid experience ARF due to sound wave scattering, leading to acoustophoretic motion. Studies by Bruus (2012b), Settnes & Bruus (2012) and Karlsen & Bruus (2015) provided an expression for ARF for ideal, viscous and thermos-viscous fluids, respectively. Recently, Doinikov *et al.* (2021a,b) derived an expression for the ARF for solid spherical particles in compressible viscoelastic fluids. Here, we aim to advance this formulation by considering the AED in micro-confinements, for particles much smaller than the acoustic wavelength. Our theory considers the particles to be solid, compressible and spherical, with the fluid's resonance frequency significantly smaller than that of the solid particles (Settnes & Bruus 2012; Karlsen & Bruus 2015). Our formulation provides new understanding of the influence of micro-confinements and viscoelasticity on the ARF and particle migration dynamics.

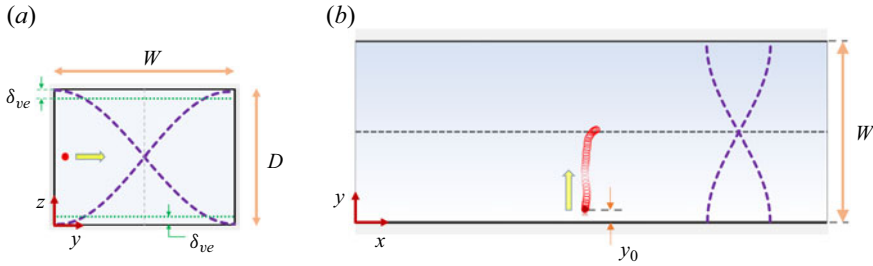


Figure 1. Schematic representation of physical domain used in the theoretical and numerical formulation. (a) Side view of the microchannel with width W and depth D , the acoustic boundary layer thickness is indicated by δ_{ve} . (b) Top view of the microchannel with particle, the starting position of the particle in the channel is y_0 . The channel width W is exposed to a one-dimensional standing wave (along y axis, shown by dashed violet lines) operating at the first harmonic mode, i.e. half-wave mode. Particle trajectory due to acoustic excitation of the fluid is shown using red circles at different time instants.

A schematic of the physical domain used in our theoretical formulation is shown in figure 1. We consider a straight rectangular microchannel of width W and depth D . The channel is filled with a viscoelastic fluid containing particles, both the particles and fluid are initially in a quiescent state. The spherical particles have radius a , density ρ_P and compressibility κ_P . The fluid has viscosity μ (with solvent and polymer contributions μ_s and μ_p , $\mu = \mu_s + \mu_p$), relaxation time τ , density ρ_0 and compressibility κ_0 . The channel is exposed to a standing bulk acoustic wave (S-BAW) along the y -axis, causing particle migration. By setting the channel width W to half the acoustic wavelength ($\lambda_0/2$), we achieve half-wave resonance. A cross-sectional view of the channel is shown in figure 1(a). In the presence of an USW, the acoustic boundary layer forms along the channel's top and bottom walls, with a thickness δ_{ve} shown in figure 1(a). Assuming the standing wave is uniform along the channel length (x -axis), we analyse fluid perturbations in the y - z plane. We consider the particle motion along the y -direction in the x - y plane, with negligible drift in the x and z directions. The initial particle position is indicated by y_0 , and a representative particle trajectory is shown in figure 1(b). We focus over a region away from the channel inlet and outlet to avoid end effects, which defines our physical domain.

2.1. Standing bulk acoustic wave and fluid perturbation

Acoustic perturbations cause changes in the pressure p , density ρ and velocity \mathbf{v} fields within a fluid. To understand these variations, we begin with the continuity and momentum equations. For a viscoelastic fluid, the governing equations are

$$\frac{\partial \rho}{\partial t} + \nabla \cdot (\rho \mathbf{v}) = 0, \quad (2.1)$$

$$\rho \left(\frac{\partial \mathbf{v}}{\partial t} + \mathbf{v} \cdot \nabla \mathbf{v} \right) = -\nabla p + \nabla \cdot \mu_s \left[\nabla \mathbf{v} + (\nabla \mathbf{v})^T - \frac{2}{3} (\nabla \cdot \mathbf{v}) \mathbf{I} \right] + \nabla \cdot \boldsymbol{\sigma}_{ve}. \quad (2.2)$$

To represent the rheological behaviour of a viscoelastic fluid, we use the Oldroyd-B model (Oldroyd 1950), where μ_s stands for the solvent viscosity, and $\boldsymbol{\sigma}_{ve}$ represents the second-order viscoelastic polymer stress tensor. Here, $\boldsymbol{\sigma}_{ve}$ incorporates both viscous and elastic effects introduced by the polymer part of the fluid and can be expressed as

$$\tau \hat{\boldsymbol{\sigma}}_{ve} + \boldsymbol{\sigma}_{ve} = \mu_p [\nabla \mathbf{v} + (\nabla \mathbf{v})^T - \frac{2}{3} (\nabla \cdot \mathbf{v}) \mathbf{I}]. \quad (2.3)$$

Here, μ_p is the contribution of the polymer viscosity to the total viscosity of the solution, $\mu = \mu_s + \mu_p$, and τ is the relaxation time. A convected time differentiation is introduced on σ_{ve} to account for the frame invariance of the stress tensor, and $\hat{\sigma}_{ve}$ represents the upper-convected stress derivative of σ_{ve} , defined as

$$\hat{\sigma}_{ve} = \frac{\partial \sigma_{ve}}{\partial t} + \mathbf{v} \cdot \nabla \sigma_{ve} - (\nabla \mathbf{v})^T \cdot \sigma_{ve} - \sigma_{ve} \cdot \nabla \mathbf{v}. \quad (2.4)$$

The governing equations (2.1)–(2.4) are nonlinear and difficult to solve directly. To simplify, we use a perturbation approach suitable for small acoustic amplitudes. Following the works of Bruus (2012b), Settles & Bruus (2012) and Doinikov *et al.* (2021a), we introduce perturbation schemes for fluid density ρ , pressure p , velocity \mathbf{v} and the viscoelastic stress tensor σ_{ve} up to second order. Unperturbed quantities are labelled with subscript ‘0’, while first- and second-order perturbations use subscripts ‘1’ and ‘2’. We assume that the zeroth-order fields remain constant in space and time. The first-order fields represent the system’s linear response to small perturbations, oscillating harmonically at an angular frequency ω and an amplitude that varies only with space (Baasch, Pavlic & Dual 2019). The second-order fields account for nonlinear interactions arising from the first-order perturbations, oscillating at double the frequency, 2ω . The perturbed fluid fields are

$$\rho = \rho_0 + \rho_1 + \rho_2, \quad p = p_0 + p_1 + p_2, \quad \mathbf{v} = \mathbf{v}_1 + \mathbf{v}_2, \quad \sigma^{ve} = \sigma_1^{ve} + \sigma_2^{ve}. \quad (2.5a-d)$$

In the unperturbed state, the viscoelastic fluid is at rest, implying that \mathbf{v}_0 and σ_0^{ve} are initially zero. We substitute equation (2.5a–d) into (2.1)–(2.4). By disregarding the products of first-order terms and keeping only the first-order terms, we express the first-order equations as

$$\frac{\partial \rho_1}{\partial t} + \rho_0 \nabla \cdot \mathbf{v}_1 = 0, \quad (2.6)$$

$$\rho_0 \frac{\partial \mathbf{v}_1}{\partial t} = -\nabla p_1 + \nabla \cdot \mu_s \left[\nabla \mathbf{v}_1 + (\nabla \mathbf{v}_1)^T - \frac{2}{3}(\nabla \cdot \mathbf{v}_1)\mathbf{I} \right] + \nabla \cdot \sigma_1^{ve}, \quad (2.7)$$

$$\tau \frac{\partial \sigma_1^{ve}}{\partial t} + \sigma_1^{ve} = \mu_p \left[\nabla \mathbf{v}_1 + (\nabla \mathbf{v}_1)^T - \frac{2}{3}(\nabla \cdot \mathbf{v}_1)\mathbf{I} \right]. \quad (2.8)$$

Furthermore, the equation of state can be expressed as

$$p_1 - p_0 = (\rho_1 - \rho_0)c_0^2, \quad (2.9)$$

where p_0 and ρ_0 are unperturbed pressure and mass density, respectively, and c_0 represents the speed of sound in the fluid.

We assume the first-order fields oscillate harmonically with an angular frequency ω (Baasch *et al.* 2019). Thus, the harmonic time dependence of the first-order field can be expressed as

$$\begin{aligned} \rho_1(r, t) &= \tilde{\rho}_1(r) e^{i\omega t}, & p_1(r, t) &= \tilde{p}_1(r) e^{i\omega t}, \\ \mathbf{v}_1(r, t) &= \tilde{\mathbf{v}}_1(r) e^{i\omega t}, & \sigma_1^{ve}(r, t) &= \tilde{\sigma}_1^{ve}(r) e^{i\omega t}. \end{aligned} \quad (2.10a-d)$$

Here, the angular frequency $\omega = 2\pi f$ and f represents the resonant frequency. The terms $\tilde{\rho}_1(r)$, $\tilde{p}_1(r)$, $\tilde{\mathbf{v}}_1(r)$ and $\tilde{\sigma}_1^{ve}(r)$ represent time-independent amplitudes (only functions of space) of first-order density, pressure, velocity and viscoelastic stress fields, respectively.

By applying harmonic time dependence (2.10a–d) to (2.6)–(2.8), we transform the first-order equations from the time domain to the frequency domain. Upon simplification, we obtain

$$i\omega\tilde{\rho}_1 + \rho_0\nabla \cdot \tilde{\mathbf{v}}_1 = 0, \tag{2.11}$$

$$i\omega\rho_0\tilde{\mathbf{v}}_1 = -\nabla\tilde{p}_1 + \nabla \cdot \mu_c[\nabla\tilde{\mathbf{v}}_1 + (\nabla\tilde{\mathbf{v}}_1)^T] - \frac{2}{3}(\nabla \cdot \tilde{\mathbf{v}}_1)\mathbf{I}, \tag{2.12}$$

where

$$\mu_c = \mu_s + \frac{\mu_p}{1 + i\tau\omega}. \tag{2.13}$$

Here, we introduce complex viscosity μ_c to describe the effect of viscoelastic parameters μ_s , μ_p and τ on the first-order fields.

The first-order fields do not contribute to the time-averaged effects (Bruus 2012b). However, the time-averaged second-order fields are non-zero. We obtain the second-order perturbed equations by substituting equation (2.5a–d) into (2.1)–(2.4) and retaining only the second-order terms. This includes the second-order perturbations of single variables as well as products of two first-order perturbations. The time-averaged second-order equations are

$$\rho_0\nabla \cdot \langle \mathbf{v}_2 \rangle = -\nabla \cdot \langle \rho_1 \mathbf{v}_1 \rangle, \tag{2.14}$$

$$\begin{aligned} \rho_0\langle \mathbf{v}_1 \cdot \nabla \mathbf{v}_1 + \mathbf{v}_1 \nabla \cdot \mathbf{v}_1 \rangle &= -\nabla\langle p_2 \rangle + \mu\nabla^2\langle \mathbf{v}_2 \rangle + \frac{\mu}{3}\nabla(\nabla \cdot \langle \mathbf{v}_2 \rangle) \\ &\quad -\tau\nabla \cdot \langle \mathbf{v}_1 \cdot \nabla \boldsymbol{\sigma}_1^{ve} \rangle + \tau\nabla \cdot \langle (\nabla \mathbf{v}_1)^T \cdot \boldsymbol{\sigma}_1^{ve} \rangle + \tau\nabla \cdot \langle \boldsymbol{\sigma}_1^{ve} \cdot \nabla \mathbf{v}_1 \rangle. \end{aligned} \tag{2.15}$$

Here, ‘ $\langle \cdot \rangle$ ’ denotes time averaging over a full oscillation period, which is $2\pi/\omega$. The time average of harmonically varying fields f and g can be expressed as $\langle f g \rangle = \frac{1}{2} \text{Re}[f \tilde{g}^c]$, where \tilde{f} and \tilde{g} are the time-independent amplitudes and c represents the complex conjugate. The last three terms on the right side of (2.15) arise from the viscoelastic fluid model and represent additional volume forces due to the fluid’s viscoelastic properties.

The time average of the second-order fields from (2.14)–(2.15) results in the primary ARF (Bruus 2012b). The ARF acting on a particle can be expressed as

$$\mathbf{F}_{rad} = \left\langle \oint_s \boldsymbol{\sigma} \cdot \mathbf{n} \, dA \right\rangle, \tag{2.16}$$

where $\boldsymbol{\sigma}$ is the total fluid stress tensor and s is the surface of the particle, \mathbf{n} is the outward normal to the surface and dA is the infinitesimal particle area. The radiation force expression can be further modified by considering the momentum flux through an arbitrary surface s_1 enclosing the particle (Doinikov *et al.* 2021b) as follows:

$$\mathbf{F}_{rad} = \left\langle \oint_{s_1} (\boldsymbol{\sigma}_2 - \rho_0\mathbf{v}_1\mathbf{v}_1) \cdot \mathbf{n} \, dA \right\rangle. \tag{2.17}$$

Here, $\boldsymbol{\sigma}_2$ is the total second-order fluid stress tensor (terms on the right side of (2.15)), which includes second-order pressure, as well as viscous and viscoelastic stresses.

Using (2.17), Doinikov *et al.* (2021a,b) derived a generalized expression for ARF on solid particles in a viscoelastic fluid. They solved first- and second-order equations near particles but did not address the effects of boundary layers at the channel walls on the ARF or the modifications in AED or ACF due to viscoelasticity. Building on their work, we present a simplified expression for ARF that includes boundary layer effects around

particles and microchannel walls for small particles (particle radius much smaller than the acoustic wavelength). We introduce a corrected ACF for viscoelastic fluids, considering first-order scattering theory and boundary layer formation, to determine the ARF and particle migration. Additionally, we analyse the impact of microchannel wall boundary layers on incoming waves and AED, incorporating viscous dissipation. This simplified expression, decoupling AED and ACF, enhances the understanding of acoustic particle migration dynamics in microchannels.

2.2. Acoustic boundary layer formation in viscoelastic fluids

Acoustic boundary layer formation at microchannel walls (Muller & Bruus 2014; Bach & Bruus 2018) and around particles (Doinikov 1997; Settnes & Bruus 2012; Karlsen & Bruus 2015) is well studied for Newtonian fluids. To modify the expression for ARF in viscoelastic fluids considering the effects of microchannel walls, understanding the acoustic boundary layer (ABL) formation on the microchannel walls is important. Here, we derive the ABL thickness in viscoelastic fluid (δ_{ve}) by solving the first-order field equations using Helmholtz decomposition (see supplementary material § 1.1 available at <https://doi.org/10.1017/jfm.2024.965>), following Doinikov *et al.* (2021a). The shear wavenumber (k_{ve}) for a viscoelastic fluid is

$$k_{ve} = (1 - i)\sqrt{\frac{\rho_0\omega}{2\mu_c}}. \quad (2.18)$$

From (2.18) the viscous boundary layer thickness δ_{ve} and viscous shear wavelength λ_{ve} for viscoelastic fluids can be expressed as (Doinikov *et al.* 2021a)

$$\delta_{ve} = -\frac{1}{\text{Im}\{k_{ve}\}} \quad \text{and} \quad \lambda_{ve} = \frac{2\pi}{\text{Re}\{k_{ve}\}}. \quad (2.19a,b)$$

Simplifying (Brown & Churchill 2009) the above expressions gives

$$\delta_{ve} = -\frac{1}{\sqrt{\Gamma} - \sqrt{\Upsilon}}, \quad (2.20)$$

$$\lambda_{ve} = \frac{2\pi}{\sqrt{\Gamma} + \sqrt{\Upsilon}}. \quad (2.21)$$

Here, Γ and Υ are functions of ς and χ , and can be expressed as

$$\Gamma = \frac{\sqrt{\varsigma^2 + \chi^2} - \varsigma}{2} \quad \text{and} \quad \Upsilon = \frac{\sqrt{\varsigma^2 + \chi^2} + \varsigma}{2}, \quad (2.22a,b)$$

where ς and χ are fluid parameters that depend on μ and τ as follows:

$$\varsigma = \frac{\rho_0\omega[\mu + \mu_s(\tau\omega)^2]}{2[\mu^2 + \mu_s^2(\tau\omega)^2]} \quad \text{and} \quad \chi = \frac{\rho_0\omega[\mu - \mu_s]\tau\omega}{2[\mu^2 + \mu_s^2(\tau\omega)^2]}. \quad (2.23a,b)$$

From here onwards we use subscript ‘v’ to indicate the viscous Newtonian fluid and ‘ve’ for the viscoelastic fluid in ABL thickness and viscous shear wavelength.

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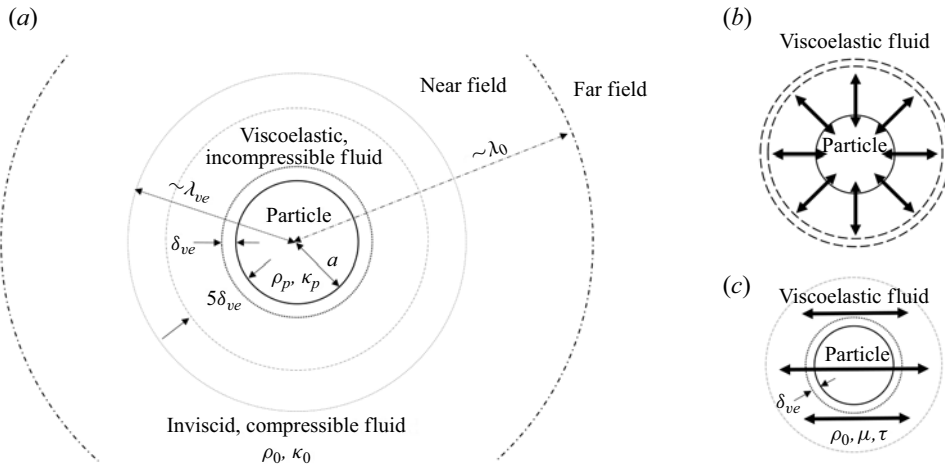


Figure 2. Schematic of (a) a solid particle of radius a in a viscoelastic fluid (viscosity μ , relaxation time τ), with particle density ρ_P and compressibility κ_P . An acoustic wave ($\phi_1 = \phi_{in} + \phi_{sc}$) is introduced to study scattering. The bulk fluid domain includes a near field ($r \ll \lambda_0$) with instantaneous scattered field ϕ_{sc} and a far field with time-retarded scattered field $\phi_{sc}(t - r/c_0)$. The viscoelastic boundary layer thickness is δ_{ve} (dotted line), with boundary layer width $\sim 5\delta_{ve}$. Beyond this, the fluid is considered inviscid and compressible with properties ρ_0 and κ_0 . A viscous shear wavelength λ_{ve} is shown by a dotted circle around the particle. (b) Compressibility contrast: particle contracts and expands in the incident pressure wave, causing monopole radiation with scattering coefficient f_1 . (c) Density contrast: particle oscillates due to inertia difference, causing dipole radiation with scattering coefficient f_2 .

2.3. Acoustic radiation force formulation

To study how viscoelastic parameters and acoustic boundary layers affect particle migration, we derive an expression for the ARF, separating the effects of the AED and the ACF, thus advancing the formulation by Doinikov *et al.* (2021b). We consider a small, compressible spherical particle (radius a , density ρ_P , compressibility κ_P) in a viscoelastic fluid (density ρ_0 , compressibility κ_0) exposed to an acoustic field with wavelength λ_0 (see figure 2). Assuming a dilute suspension and treating particles as weak scatterers ($a \ll \lambda_0$), we set the system's frequency below the particle's resonance frequency due to a higher speed of sound in the particle compared with that in the fluid.

We actuate the walls of a viscoelastic fluid-filled microchannel at the system's resonance frequency (see figure 1). This generates pressure and velocity perturbations in the fluid, which act as incoming waves for the particle, represented by p_{in} and v_{in} . The amplitudes of these waves vary with the fluid's viscoelastic properties and ABL formation at the channel walls, and are obtained through numerical simulations (see § 3). In theory, we denote the incoming and scattered waves as ϕ_{in} and ϕ_{sc} , respectively, with the total field $\phi_1 = \phi_{in} + \phi_{sc}$. The velocities are given by $\mathbf{v}_{in} = \nabla\phi_{in}$ for the incoming wave, $\mathbf{v}_{sc} = \nabla\phi_{sc}$ for the scattered wave and $\mathbf{v}_1 = \mathbf{v}_{in} + \mathbf{v}_{sc}$ for the first-order velocity. Figure 2(a) shows the acoustic wavelength λ_0 , boundary layer thickness δ_{ve} and viscous shear wavelength λ_{ve} , comparing the scales of the incoming compressible and scattered shear waves. A spherical coordinate system (r, θ, φ) is used for the analysis.

In response to external acoustic perturbations, the fluid's behaviour changes radially from the particle's surface, forming three distinct regions. In the boundary layer region ($a < r \lesssim a + 5\delta_{ve}$), viscoelastic properties dominate due to high shear gradients. Here, the fluid is considered to be incompressible because the wave propagation time through the boundary layer is much shorter than the acoustic wave's oscillation period

($5\delta_{ve}/c_0 \ll 1/\omega$). Field variations in this region exhibit an exponential decay, falling below 1% at a distance of $5\delta_{ve}$. We use this distance to differentiate between the boundary layer and near-field region (discussed in supplemental material § 1), and the exact value of the prefactor is not critical in our analysis. The near-field region is defined as $a + 5\delta_{ve} \lesssim r \ll \lambda_0$ and the far-field region as $r \gg \lambda_0$, with the fluid considered inviscid and compressible in both the regions.

We characterize the acoustic wave scattering from a point scatterer using a time-retarded multipole expansion. In the far-field region (see figure 2a), only monopole (ϕ_{mp}) and dipole (ϕ_{dp}) components are significant and take the forms $\phi_{mp}(r, t) = b(t - r/c_0)/r$ and $\phi_{dp}(r, t) = \nabla \cdot [\mathbf{B}(t - r/c_0)/r]$, where b and \mathbf{B} are functions of $(t - r/c_0)$ (Bruus 2012b; Settnes & Bruus 2012). The scalar function b is related to the first-order density field ($b \sim \rho_{in}$), and the vector function \mathbf{B} corresponds to the first-order velocity field ($\mathbf{B} \sim \mathbf{v}_{in}$). Thus, in the far field, the total scattering field $\phi_{sc} \approx \phi_{mp} + \phi_{dp}$, can be expressed as

$$\phi_{sc}(r, t) = -f_1 \frac{a^3}{3\rho_0} \frac{\partial_t \rho_{in}(t - r/c_0)}{r} - f_2 \frac{a^3}{2} \nabla \cdot \left[\frac{\mathbf{v}_{in}(t - r/c_0)}{r} \right]. \quad (2.24)$$

Here, f_1 is the monopole scattering coefficient and f_2 is the dipole scattering coefficient. To maintain the correct dimensions of ϕ_{sc} , we introduce a , ρ_0 and ∂_t in (2.24). In the near-field region $a + 5\delta_{ve} \lesssim r \ll \lambda_0$, the scattering field depends on the instantaneous argument t , unlike the time-retarded argument in the far field (Bruus 2012b; Settnes & Bruus 2012). Thus, the total scattered field becomes

$$\phi_{sc}(r, \theta) = \phi_{mp}(r) + \phi_{dp}(r, \theta) = -f_1 \frac{a^3}{3\rho_0} \partial_t \rho_{in} \frac{1}{r} + f_2 \frac{a^3}{2} v_{in} \frac{\cos \theta}{r^2}. \quad (2.25)$$

The first-order velocity and pressure field can be expressed as

$$\mathbf{v}_1 = \nabla \phi_1 = \nabla \phi_{in} + \nabla \phi_{sc}, \quad p_1 = -\rho_0 \partial_t \phi_1 = -i\rho_0 \omega (\phi_{in} + \phi_{sc}). \quad (2.26a,b)$$

We calculate the ARF using (2.17) for an arbitrary surface in the far-field region. Here, the fluid is inviscid, therefore viscous and viscoelastic stresses are zero, and σ_2 simplifies to the time-averaged second-order pressure: $\langle p_2 \rangle = \kappa_0 \langle p_1^2 \rangle / 2 - \rho_0 \langle v_1^2 \rangle / 2$, similar to Settnes & Bruus (2012). Using the incoming and far-field scattered fields (2.26a,b), we derive the ARF expression (see supplemental material § 1.2), which simplifies as follows:

$$\mathbf{F}_{rad} = -\nabla U_{rad}, \quad (2.27)$$

$$U_{rad} = \frac{4\pi}{3} a^3 \left[f_1 \frac{\kappa_0}{2} \langle p_{in}^2 \rangle - f_2 \frac{3\rho_0}{4} \langle v_{in}^2 \rangle \right]. \quad (2.28)$$

Here, U_{rad} is the acoustic potential, f_1 and f_2 are unknowns that need to be determined for the case of viscoelastic fluid to predict the ARF.

When a fluid with a particle is subjected to pressure oscillations, the particle compresses and expands. If the particle's compressibility differs from that of the fluid, it generates fluid flow towards or away from the particle (Challis *et al.* 2005). For a small spherical particle, this resembles a monopole source, where a more compressible particle ejects fluid at a rate of $\partial_t m$, calculated using the scattered first-order velocity field $\rho \mathbf{v}_{sc}$ (Bruus 2012b; Settnes & Bruus 2012; Karlsen & Bruus 2015). Following Settnes & Bruus (2012), we find that viscoelasticity does not affect the monopole scattering coefficient f_1 (see supplemental material § 1.3). Therefore, f_1 can be expressed as

$$f_1(\kappa_p^*) = 1 - \kappa_p^*. \quad (2.29)$$

Here, κ_p^* is the compressibility ratio between particle and viscoelastic fluid, $\kappa_p^* = \kappa_p/\kappa_0$.

The dipole scattering coefficient f_2 arises from the density difference between the particle and the surrounding fluid (Bruus 2012b). For denser particles, pressure waves cause oscillatory motion due to inertia differences (Challis *et al.* 2005). This motion is influenced by the viscous boundary layer (Settnes & Bruus 2012). In this study, we present a new expression for f_2 that includes both viscous and elastic effects of the fluid, which were not considered in previous studies (Doinikov *et al.* 2021a,b). The value of f_2 is determined through asymptotic matching of the velocity in the ABL with the near-field region, as detailed in supplemental material § 1.3. Therefore, f_2 can be expressed as

$$f_2(\rho_p^*, \delta_{ve}^*, \lambda_{ve}^*) = \frac{2[1 - \gamma^*(\delta_{ve}^*, \lambda_{ve}^*)](\rho_p^* - 1)}{2\rho_p^* + 1 - 3\gamma^*(\delta_{ve}^*, \lambda_{ve}^*)}, \quad (2.30)$$

$$\gamma^*(\delta_{ve}^*, \lambda_{ve}^*) = \frac{3(1 + i)[1 + Q + i(1 + P)]}{(P - iQ)^2}, \quad (2.31)$$

and P and Q become

$$P = \frac{1}{\delta_{ve}^*} + \frac{2\pi}{\lambda_{ve}^*} \quad \text{and} \quad Q = \frac{1}{\delta_{ve}^*} - \frac{2\pi}{\lambda_{ve}^*}. \quad (2.32a,b)$$

Here, δ_{ve}^* and λ_{ve}^* are the dimensionless ABL thickness and viscous shear wavelength in a viscoelastic fluid, defined as $\delta_{ve}^* = \delta_{ve}/a$ and $\lambda_{ve}^* = \lambda_{ve}/a$. The density ratio between the particle and fluid is represented by $\rho_p^* = \rho_p/\rho_0$. The dipole scattering coefficient f_2 depends on δ_{ve}^* and λ_{ve}^* , which are functions of the viscoelastic parameters μ_s , μ_p and τ , as obtained from (2.20) and (2.21). In the absence of elasticity, for a viscous fluid, $\lambda_{ve}/\delta_{ve} = \lambda_v/\delta_v = 2\pi$, matching the results of Settnes & Bruus (2012). For an ideal fluid with zero viscosity ($\delta_{ve}^* = 0$ and $\lambda_{ve}^* = 0$), (2.30) simplifies to $f_2 = 2(\rho_p^* - 1)/(2\rho_p^* + 1)$, as established by Gorkov (1962).

For an ideal fluid, in a microchannel exposed to a one-dimensional (1-D) S-BAW of the form $\tilde{p}_{in} = p_a \cos(k_y y)$ with $\lambda_0 \gg a$, the expression for the ARF (equation 2.27) simplifies to (Yosioka 1955; Gorkov 1962; Bruus 2012b)

$$F_{rad} = 4\pi\Phi(\kappa_p^*, \rho_p^*)a^3k_yE_{ac} \sin(2k_y y), \quad \Phi(\kappa_p^*, \rho_p^*) = \frac{1}{3}f_1(\kappa_p^*) + \frac{1}{2}f_2^r(\rho_p^*). \quad (2.33a,b)$$

Here, Φ , a , k_y and E_{ac} denote the ACF, particle radius, wavenumber and AED, respectively. The compressibility and density ratios are represented by $\kappa_p^* = \kappa_p/\kappa_0$ and $\rho_p^* = \rho_p/\rho_0$. The value of E_{ac} is independent of fluid properties and is given by $E_{ac} = p_a^2/(4\rho_0^2c_0^2)$. Settnes & Bruus (2012) modified the expression for F_{rad} for a viscous fluid by correcting the ACF (Φ) to account for the acoustic boundary layer thickness δ_v , which depends on fluid viscosity.

Our study considers a rectangular channel with a 1-D S-BAW (see figure 1). The channel width is set to $\lambda_0/2$ to achieve resonance with a unidirectional pressure wave, which serves as the incoming wave for the particle. The incoming wave is assumed to be in resonance, and has the form $\tilde{p}_{in} = p_a^{ve} \cos(k_y y)$, and the AED is $E_{ac}^{ve} = (p_a^{ve})^2/4\rho_0^2c_0^2$. Here, p_a^{ve} is the amplitude of the incoming pressure field generated inside the microchannel which varies with viscoelastic parameters. The wavenumber along the y direction is $k_y = 2\pi/\lambda_0$. Following the works of Yosioka (1955) and Settnes & Bruus (2012), we modify the expression for the ARF incorporating the viscoelastic parameters,

$$F_{rad} = 4\pi\Phi(\kappa_p^*, \rho_p^*, \delta_{ve}^*, \lambda_{ve}^*)a^3k_yE_{ac}^{ve} \sin(2k_y y), \quad (2.34)$$

$$\Phi(\kappa_p^*, \rho_p^*, \delta_{ve}^*, \lambda_{ve}^*) = \frac{1}{3}f_1(\kappa_p^*) + \frac{1}{2}f_2^r(\rho_p^*, \delta_{ve}^*, \lambda_{ve}^*). \quad (2.35)$$

The ACF (Φ) for viscoelastic fluids depends on δ_{ve}^* , λ_{ve}^* , ρ_p^* and κ_p^* . Here, $\delta_{ve}^* = \delta_{ve}/a$ and $\lambda_{ve}^* = \lambda_{ve}/a$. However, δ_{ve} and λ_{ve} are functions of the viscoelastic parameters (μ_s , μ_p , τ), ρ_0 and ω , as given by (2.20) and (2.21). We compute Φ by substituting equation (2.29) and the real part of (2.30) into (2.35). Further, we refine the AED for viscoelastic fluids by accounting for boundary layer effects at the channel walls, given by $E_{ac}^{ve} = (p_a^{ve})^2/(4\rho c_0^2)$. The amplitude of acoustic pressure in the viscoelastic fluid p_a^{ve} , which depends on μ and τ , is determined through numerical simulations detailed in § 3. In summary, we derived an expression for the ARF in viscoelastic fluids by decoupling the effects of viscoelasticity on Φ and E_{ac}^{ve} , particularly for $a \ll \lambda_0$, contrasting the approach taken by Doinikov *et al.* (2021*a,b*). This new expression for ARF enhances our understanding of the effects of fluid viscoelasticity on the AED and ACF and consequently the particle migration dynamics.

2.4. Acoustic particle migration characteristics

We present a new formulation for particle migration in a viscoelastic fluid under ultrasonic excitation. A particle in a viscoelastic fluid experiences several forces: ARF, inertial force, viscoelastic force and drag force. The ARF varies along the direction of the standing wave, and is proportional to $\sin(2k_y y)$ (see (2.34)). Besides ARF, inertial force can also influence particle migration; however, a comparison of the acceleration time scale ($\tau_a = (4/3)\pi a^3 \rho_p / 6\pi \mu a$) and the translation time scale ($\tau_{trans} = W/2V_P$) reveals that the acceleration time scale (10^{-6} s) is much smaller than the translation time scale (10^{-2} s), allowing us to neglect inertial effects (Muller *et al.* 2013). Here, V_P is the particle velocity. In viscoelastic flows, particle migration arises from the imbalance in the first normal stress difference, $N_1(\dot{\gamma}) = \sigma_{xx} - \sigma_{yy}$, and the viscoelastic force (F_e) is expressed as (Leshansky *et al.* 2007) $F_e \sim a^3(\partial N_1(\dot{\gamma})/\partial y)$. However, we consider a quiescent fluid with a negligible strain rate ($\dot{\gamma}$) and therefore F_e is taken to be zero.

With inertial and viscoelastic forces negligible, particle migration is governed by the balance of ARF and drag force that can be explained in a Lagrangian framework. Our study focuses on particles with a diameter of 15 μm ($\beta = a/(W/2) = 0.0375$). Stokes drag due to acoustic streaming is significant for submicron particles, while the ARF dominates for particles of diameter above 2 μm (Lighthill 1978; Barnkob *et al.* 2010; Muller *et al.* 2012). Consistent with this, our experiments did not show any traces of acoustic flow rolls, allowing us to neglect the influence of Stokes drag arising from acoustic streaming. We introduce an ordinary differential equation to express Newton's law of motion for the particle. If m is the mass of a particle, V_P is the particle velocity at position y and the different forces are represented by $F_i(y)$, a force balance on the particle gives

$$m \frac{dV_P}{dt} = \sum_i F_i(y). \tag{2.36}$$

Neglecting the inertial, gravitational (Barnkob *et al.* 2010) and viscoelastic forces, (2.36) reduces to

$$F_{drag} = F_{rad}. \tag{2.37}$$

Due to the inherent viscoelastic properties of the fluid, there is a change in the drag coefficient and the correction in the drag coefficient for a spherical particle has been reported by Faroughi *et al.* (2020). Thus, the drag force in a viscoelastic fluid can be

expressed as

$$F_{drag} = 6\pi\mu a\xi V_p. \quad (2.38)$$

Here, ξ represents the drag coefficient correction. For a quiescent fluid considered in our study, $\xi \approx 1$ (Faroughi *et al.* 2020). Incorporating equations (2.34) and (2.38) in (2.37) gives

$$6\pi\mu a\xi \frac{dy}{dt} = 4\pi\Phi(\kappa_p^*, \rho_p^*, \delta_{ve}^*, \lambda_{ve}^*) a^3 k_y E_{ac}^{ve} \sin(2k_y y). \quad (2.39)$$

By simplifying equation (2.39), we obtain

$$V_p = \frac{2\Phi(\kappa_p^*, \rho_p^*, \delta_{ve}^*, \lambda_{ve}^*) k_y a^2 E_{ac}^{ve} \sin(2k_y y)}{3\mu\xi}. \quad (2.40)$$

Integrating the equation via separation of variables y and t gives the analytical expression for the particle trajectory, which is expressed as

$$y(t) = \frac{1}{k_y} \arctan \left\{ \tan[k_y y(0)] \exp \left[\frac{4\Phi(\kappa_p^*, \rho_p^*, \delta_{ve}^*, \lambda_{ve}^*) (k_y a)^2 E_{ac}^{ve} t}{3\mu\xi} \right] \right\}. \quad (2.41)$$

Here, $y(0)$ and $y(t)$ are the initial location and particle location at a time instant t , respectively. We obtain an expression for the particle migration time by adjusting (2.41) as

$$t = \frac{3\mu\xi}{4\Phi(\kappa_p^*, \rho_p^*, \delta_{ve}^*, \lambda_{ve}^*) (k_y a)^2 E_{ac}^{ve}} \ln \left[\frac{\tan[k_y y(t)]}{\tan[k_y y(0)]} \right]. \quad (2.42)$$

We validate the theory described above using experiments, and the details are given in §4.

3. Numerical simulations

We perform numerical simulations to determine acoustic field perturbations in the viscoelastic fluid inside the microchannel considering the boundary layer formation on the channel walls. These perturbations act as incoming waves to suspended particles and represent the AED in the fluid. Assuming a 1-D S-BAW along the y -direction (figure 1a), we consider the variation of the acoustic field and AED along the length (x -direction) of the channel to be negligible. Therefore, we select the channel cross-section in the y - z plane as the simulation domain. Similar to the experimental device, the domain of width 400 μm and depth 300 μm is filled with a viscoelastic fluid specified by μ_s , μ_p and τ .

We numerically solve (2.11)–(2.13) for the cross-section of the microchannel, excluding particles, using the finite element method in COMSOL Multiphysics 6.0. A detailed description of the numerical model is presented in supplemental material §2. The channel sidewalls are excited with a velocity boundary condition, $\tilde{v}_1 = iA\omega\hat{e}_y$ in the frequency domain (Bach & Bruus 2018; Vargas *et al.* 2022). Here, A is the vibration amplitude, determined through 3-D numerical modelling of the experimental device (Barnkob *et al.* 2010; Dual & Möller 2012; Dual & Schwarz 2012; Hahn *et al.* 2015). The angular frequency $\omega = 2\pi f$, where $f \approx 1.93$ MHz is the resonant frequency of the experimental device. The top and bottom walls have a Lagrangian no-slip boundary condition. The first-order fields (\tilde{p}_1, \tilde{v}_1) in the channel act as incoming waves for the particles, thus we denote the perturbations inside the fluid as \tilde{p}_{in} and \tilde{v}_{in} . Due to half-wave resonance condition, the incoming pressure wave distribution is $\tilde{p}_{in} = p_a^{ve} \cos(k_y y)$, the

Solutions	C [wt.%]	μ [mPa s]	τ [s]	$\mu^* = \mu/\mu_{bf}$	$De = \tau\omega$
Newtonian	0.00	1.69	0	1.90	0
PVP (0.36 MDa)	0.10	1.69	7.49×10^{-6}	1.90	91
PEO (0.40 MDa)	0.20	1.69	1.46×10^{-5}	1.90	178

Table 1. Concentration and viscoelastic properties of various fluids, the Newtonian fluid is DI water+0.3 wt.% glycerol. For all of the fluids: $\mu_{bf} = 0.89$ mPa s, $\rho^* = \rho_0/\rho_{bf} \approx 1.007$ and $c^* = c_0/c_{bf} \approx 1.003$ (Rouse 1953; Zimm 1956; Tirtaatmadja, McKinley & Cooper-White 2006).

amplitude of pressure field p_a^{ve} is given by \tilde{p}_{in} at the sidewall (at $y = 0$). By following the approach for 1-D S-BAW wave in microchannels (Barnkob *et al.* 2010; Bruus 2012b; Karlsen & Bruus 2015), we find AED using $E_{ac}^{ve} = (p_a^{ve})^2/4\rho c_0^2$, where p_a^{ve} depends on the fluid’s viscoelastic properties.

We conduct a mesh convergence study following Muller & Bruus (2014). The mesh convergence parameter, C_M , for a solution g with respect to a reference solution g_{ref} is defined as $C_M(g) = [\int (g - g_{ref})^2 dy dz / \int (g_{ref})^2 dy dz]^{1/2}$. We choose $C_M = 10^{-3}$, and select the mesh by ensuring δ_{ve}/d_{bd} is greater than 1 at which both the first- and second-order fields converge. Here, d_{bd} is the mesh size in the boundary layer. We validate the numerical model for both first- and second-order fluid fields against Hintermuller *et al.* (2017), which shows close agreement (see supplemental material § 2.1). We also predict the ARF using a numerical model (Baasch *et al.* 2019) and compare it with the theoretical predictions (supplemental material § 2.1). The predicted acoustic perturbations and ARF are also validated with existing studies (Hintermuller *et al.* 2017; Doinikov *et al.* 2021a) (see supplemental material § 2.2).

4. Experimental

Experiments are performed with dilute suspensions containing spherical polystyrene particles of size between 5 and 25 μm (microParticles GmbH, Berlin) in viscoelastic and Newtonian fluids. Polyvinylpyrrolidone (PVP) solution, which is a pure viscoelastic fluid of molecular weight 0.36 MDa, (Sigma-Aldrich, USA) and polyethylene oxide (PEO) solution which is a shear-thinning viscoelastic fluid (Sigma-Aldrich, USA) of molecular weights 0.4 and 1.0 MDa are used as viscoelastic fluids. The details of the viscoelastic fluid preparation are given in supplemental material § 3.1. A mixture of deionized (DI) water and 0.3% glycerol (Sigma-Aldrich, Bangalore, India) is used as the Newtonian fluid. In both viscoelastic and Newtonian fluids, Iodixanol (OptiPrep™, Sigma-Aldrich, Bangalore, India) is mixed to adjust the fluid density. The proportions are carefully tuned to avoid significant a difference in density and speed of sound between the viscoelastic and Newtonian fluids. The properties of the fluids are presented in table 1. The fluid viscosity is measured using a rotational rheometer (MCR 72, Anton-Paar). The relaxation time τ of dilute viscoelastic fluids are predicted using available correlations (Rouse 1953; Zimm 1956). Other viscoelastic fluid properties and details about the relaxation time measurement is given in supplemental material § 3.1.

A schematic diagram of the experimental set-up is shown in figure 3(a). The glass–silicon–glass microchip (see figure 3b) is fabricated by photolithography followed by dry reactive ion etching. First, the channel design is patterned on a 3 inch (100) silicon wafer of 300 μm thickness by coating the wafer with a positive photoresist (MICROPOSIT

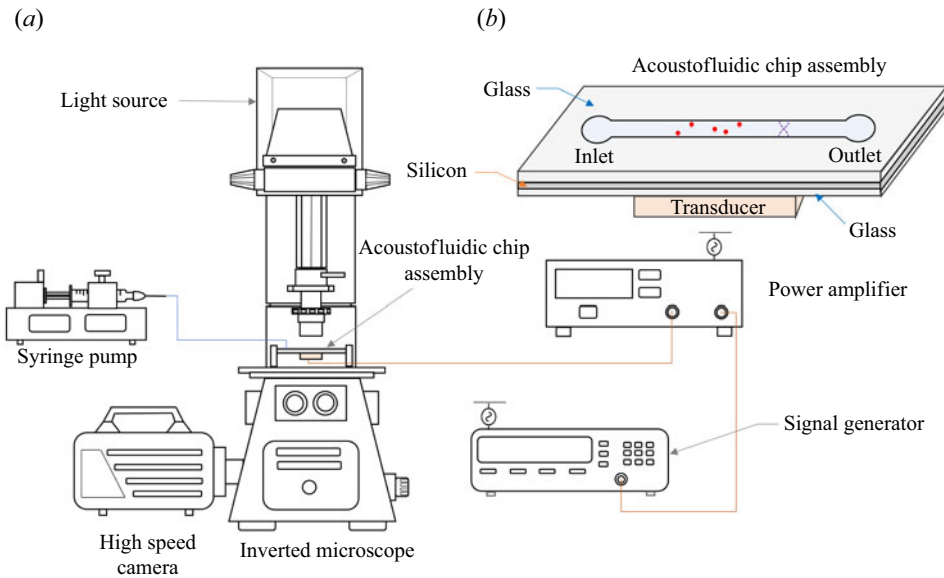


Figure 3. Schematic of (a) experimental set-up, (b) acoustofluidic chip assembly.

S1813), followed by UV exposure. The patterned wafer is through etched to realize a channel layer of 20 mm length having a rectangular cross-section of 400 μm width (W) and 300 μm depth (D). The channel is sealed with two borosilicate glasses of 500 μm thickness on top and bottom sides using anodic bonding by applying a voltage of 1000 V and temperature of 450 $^{\circ}\text{C}$. Inlet and outlet holes are micro-drilled to establish fluidic connections.

The working fluid containing suspended particles is infused into the channel using a syringe pump (neMESYS pump, Cetoni GmbH, Germany). The microchannel is actuated using a piezoelectric transducer (2.0 MHz, Sparkler Piezoceramics) attached to the bottom glass lid using an epoxy with a sinusoidal signal generated from a function generator (SMC100A, Rohde Schwarz, Germany) and amplified using an amplifier (75A250A, Amplifier Research, USA) operating between 10 and 1000 mW.

The resonance frequency of the system is identified by introducing a 15 μm spherical polystyrene particle suspension inside the channel and actuating the transducer between 1.85 and 2.1 MHz. At half-wave resonance condition, the particles quickly migrate to the nodal plane (Nath *et al.* 2021) at the channel centre. The resonant frequency of the system is found to be 1.93 MHz, which is maintained throughout the study. We measure the AED for the base fluid at the resonance frequency using a particle tracking method (Barnkob *et al.* 2010), and find it to be 48.3 J m^{-3} . The lateral migration of particles is observed using an inverted microscope (IX73, Olympus) coupled with a high-speed CCD camera (SA5, Photron) operating at 500 fps. The particle trajectory and velocity are determined by analysing the captured videos using a free video analysis and modelling tool, tracker 6.1.0.

5. Results and discussion

We study the effect of fluid viscoelasticity on the acoustic field and subsequently the transport dynamics of particles in microchannels of dimensions comparable to the acoustic

wavelength ($D \sim W \sim \lambda_0$). In § 5.1, we report the behaviour of a viscoelastic fluid in a rectangular microchannel exposed to a S-BAW, where the fluid perturbations are influenced by the ABL on the microchannel walls. Then, we present and discuss the effects of ABL and the viscoelastic parameters of the fluid on the AED in § 5.2. Using theoretical formulations, we decouple the effects of AED on the ARF. We report the effects of fluid viscoelasticity and the AED on the ARF in § 5.3. The magnitude and distribution of the ARF in the fluid and the resulting particle migration dynamics are discussed in § 5.4. Here, we decouple the viscous and elastic effects on the acoustic force field and particle migration by studying the individual effects of μ_p and μ_s (with $\mu = \mu_p + \mu_s$) and τ . Our study mainly addresses the effects of viscoelasticity and boundary layer formation at the microchannel walls on particle migration, which is missing in the literature. In our analysis, we non-dimensionalize the viscoelastic parameters: solvent viscosity (μ_s) via dimensionless solvent viscosity $\mu_s^* = \mu_s/\mu_{bf}$, polymer viscosity (μ_p) via dimensionless polymer viscosity $\mu_p^* = \mu_p/\mu_{bf}$ and relaxation time (τ) via the Deborah number $De = \tau\omega$. Here, μ_{bf} is the base Newtonian fluid (DI water) viscosity, and ω is the angular frequency, which is kept constant throughout the study. Similarly, the dimensionless complex viscosity, density and speed of sound of the fluid are taken as, $\mu_c^* = \mu_c/\mu_{bf}$, $\rho^* = \rho_0/\rho_{bf}$ and $c^* = c_0/c_{bf}$, respectively.

5.1. Effect of viscoelastic properties on fluid perturbations

A S-BAW induces perturbations in the viscoelastic fluid present in the microchannel. We analyse the variation of the first-order fields (\tilde{p}_1, \tilde{v}_1) along the channel width (y -direction) (refer to figure 1a) and depth (z -direction) in the absence of particles by numerically solving (2.11)–(2.13), as detailed in § 2.3. These perturbed fields act as incoming fields for the particle, hence we name them as p_{in} and v_{in} . Here, v_{in} indicates the component of perturbed velocity field along the y -direction. The perturbed fields are characterized using dimensionless first-order fluid pressure, $p_{in}^* = \tilde{p}_{in}/(\rho_0 c_0 A \omega)$, and dimensionless first-order fluid velocity, $v_1^* = \tilde{v}_{in}/(A \omega)$ (Vargas *et al.* 2022), where A is the amplitude of vibration of the channel, and ρ_0 and c_0 are respectively the density and speed of sound of the viscoelastic fluid. The variations of the incoming fields are shown in figure 4. Here, $y^* = y/(W/2)$ and $z^* = z/(D/2)$. We compare the field fluctuations in a viscoelastic fluid for $De = 0.1, 1.0, 10, 300$ and 10^5 with those in a Newtonian fluid ($De = 0$), for a fixed total viscosity ($\mu^* = 1001$, with $\mu_p^* = 1000$ and $\mu_s^* = 1$), density ($\rho^* = 1$) and speed of sound ($c^* = 1$), thereby decoupling the elastic effects from the viscous effects.

We depict the distribution of p_{in}^* along the channel width y^* in figure 4(a), where its magnitude varies from a maximum at the channel walls ($y^* = 0$ or $y^* = 2$) to zero at the channel centre ($y^* = 1$). A zero value of p_{in}^* indicates a pressure node, signifying the absence of the primary ARF. In contrast, v_{in}^* attains a maximum at the centre and decreases to zero at the walls, suggesting a velocity node at the walls, as shown in figure 4(b). The fluid field variation along z^* is symmetric about the channel centre $z^* = 1$. A decrease in p_{in}^* from the wall ($z^* = 0$) to the centre ($z^* = 1$) is seen in figure 4(c), while figure 4(d) depicts oscillations in v_{in}^* near the wall that stabilize at the centre. These fluctuations can be attributed to viscous shear disturbances and acoustic boundary layer formation resulting from the no-slip condition at the walls and acoustic perturbations (Hamilton, Ilinskii & Zabolotskaya 2003; Baasch & Dual 2018). Specifically, the ABLs formed at the top and bottom walls of the microchannel (shown in figure 1a) affect the pressure and velocity distribution along the z -direction. A change in nature of shear waves near particles with viscoelastic parameters has been reported by Doinikov *et al.* (2021a). However, in their

Fluid viscoelasticity affects ultrasound force field

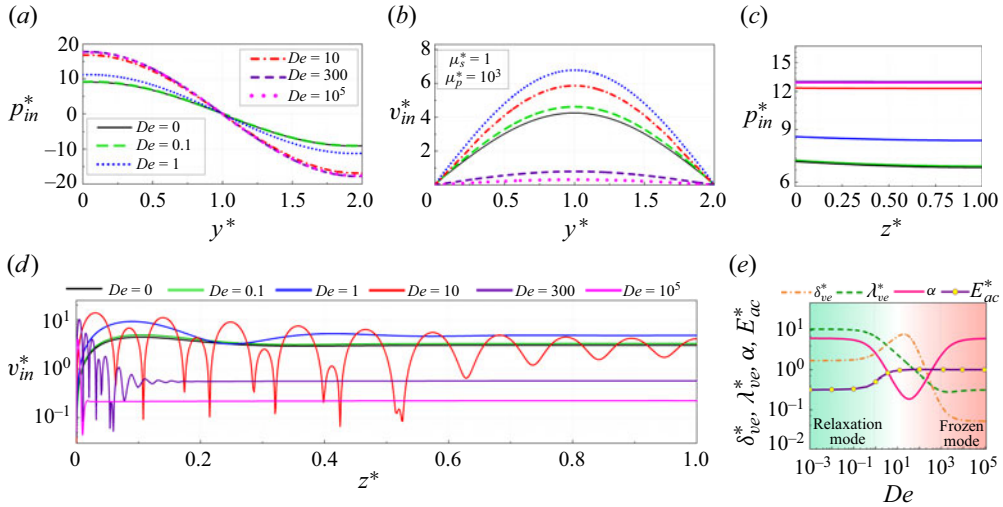


Figure 4. Numerical results of dimensionless incoming pressure (p_{in}^*) and velocity (v_{in}^*) fields in Newtonian ($De = 0$) and viscoelastic fluids ($De = 0.1, 1, 10, 300, 10^5$) at $\mu_p^* = 1000$, $\mu_s^* = 1$, $\rho^* = 1$ and $c^* = 1$. Variation of (a) p_{in}^* along y^* (along width or S-BAW direction, at $z^* = 1$), (b) v_{in}^* along y^* ($y^* = 0$ and 2 as the channel walls, $y^* = 1$ as the centre), (c) p_{in}^* along z^* (along depth or perpendicular to S-BAW, at $y^* = 0.5$) and (d) v_{in}^* along z^* (symmetric about the channel centre $z^* = 1$, $z^* = 0$ is the channel wall perpendicular to S-BAW direction), refer to figure 1. (e) Theoretical and numerical variation of dimensionless boundary layer thickness (δ_{ve}^*), viscous shear wavelength (λ_{ve}^*), α ($\lambda_{ve}^*/\delta_{ve}^*$) and E_{ac}^* with De .

study, the discussion is limited to the effect of boundary layer formation on a particle in a viscoelastic fluid from the perspective of acoustic streaming. Here, we study the effects of viscoelasticity on the incoming waves and unravel the effects of boundary layer formation at the channel walls on the perturbations.

Here, the viscous shear disturbances propagate from the walls to the bulk, in the z -direction, i.e. perpendicular to the S-BAW direction, influenced by the fluid properties. The characteristics of viscous shear waves with De are shown in figure 4(e), where the viscous shear wave is characterized using the dimensionless boundary layer thickness ($\delta_{ve}^* = \delta_{ve}/a$) and the dimensionless viscous shear wavelength ($\lambda_{ve}^* = \lambda_{ve}/a$). The parameter δ_{ve}^* indicates the penetration distance of viscous disturbances, while λ_{ve}^* provides an idea about the wavelength of shear waves or the number of oscillations in the vicinity of the channel wall, as obtained from (2.20) and (2.21). In the absence of elasticity ($De \approx 0$) or in low elasticity fluids (at very low values of $De = 0.1$), the shear waves attenuate easily due to higher viscous effects, and oscillations are overdamped (shown in figure 4(d), indicated by a smaller δ_{ve}^* and larger λ_{ve}^* ($\lambda_{ve}^* > \delta_{ve}^*$) in figure 4(e)). Here, $\varsigma = \rho_0\omega/(2\mu_{bf}\mu^*)$ and $\chi = 0$ (2.23a,b). From (2.13), (2.20) and (2.21), the dimensionless complex viscosity $\mu_c^* (= \mu_c/\mu_{bf})$, δ_{ve}^* and λ_{ve}^* reduce to

$$\mu_c^*|_{De \rightarrow 0} = \mu_s^* + \mu_p^*, \quad \delta_{ve}^*|_{De \rightarrow 0} = \frac{1}{a} \sqrt{\frac{2\mu_{bf}(\mu_s^* + \mu_p^*)}{\rho_0\omega}} \quad \text{and} \quad \lambda_{ve}^*|_{De \rightarrow 0} = 2\pi\delta_{ve}^*. \quad (5.1a-c)$$

As De increases to intermediate values ($De = 1.0$ and 10) or in moderate elasticity fluids, the amplitude, frequency and propagation distance of viscous shear waves increase due to the transition from a viscous to an elastic state. This transition is shown by the variation of v_{in}^* over a larger distance from the channel wall in figure 4(d). Further, as

depicted in figure 4(e), there is an increase in δ_{ve}^* and a decrease in λ_{ve}^* , with δ_{ve}^* being greater than λ_{ve}^* . Here, μ_c^* , ζ and χ reduce to

$$\mu_c^*|_{De} = \mu_s^* + \frac{\mu_p^*}{1 + iDe}, \tag{5.2a-c}$$

$$\zeta|_{De} = \frac{\rho_0\omega[\mu^* + \mu_s^*De^2]}{2\mu_{bf}[\mu^{*2} + \mu_s^{*2}De^2]} \quad \text{and} \quad \chi|_{De} = \frac{\rho_0\omega[\mu^* - \mu_s^*]De}{2\mu_{bf}[\mu^{*2} + \mu_s^{*2}De^2]}.$$

By substituting the above values of ζ and χ into (2.20) and (2.21), we obtain the variation of δ_{ve}^* and λ_{ve}^* for intermediate De values.

At a higher De or for high elasticity fluids, disturbances attenuate faster with further increases in De ($De = 300$ and 10^5) due to a decrease in the contribution of μ_p^* to μ_c^* , as indicated by a decrease in δ_{ve}^* in figure 4(d), which stabilizes at higher De values. At very high De ($= 10^5$), the polymer contribution to the complex viscosity approaches zero, restricting the propagation of viscous shear waves to a smaller distance from the wall, indicated by variations in v_{in}^* very close to the wall in figure 4(d) and negligible variation of δ_{ve}^* and λ_{ve}^* with De in figure 4(e), where $\lambda_{ve}^* > \delta_{ve}^*$. Here, $\zeta = \rho_0\omega/(2\mu_{bf}\mu_s^*)$ and $\chi = 0$. The values of μ_c^* , δ_{ve}^* and λ_{ve}^* reduce to

$$\mu_c^*|_{De \rightarrow \infty} = \mu_s^*, \quad \delta_{ve}^*|_{De \rightarrow \infty} = \frac{1}{a} \sqrt{\frac{2\mu_{bf}\mu_s^*}{\rho_0\omega}} \quad \text{and} \quad \lambda_{ve}^*|_{De \rightarrow \infty} = 2\pi\delta_{ve}^*. \tag{5.3a-c}$$

The variation in amplitude of v_{in}^* along y^* and z^* shows a non-monotonic pattern with increasing De , as shown in figures 4(b) and 4(d). At low De ($De \leq 1$), higher momentum transfer to the fluid occurs with increasing De or elasticity, causing an increase in v_{in}^* . Beyond $De = 1$, due to a significant reduction in effective viscosity, v_{in}^* decreases. Our results in figures 4(a) and 4(c) illustrate an increase in pressure amplitude of incoming waves from $De = 0$ to $De = 300$ at a fixed μ^* , followed by a small decrease and then negligible variation with further increases in De . However, the rate of increase in p_{in}^* with De is minimal for fluids with low elasticity ($De \ll 1$), more pronounced for fluids with moderate elasticity (intermediate De) and negligible for fluids with high elasticity ($De = 10^5$). Interestingly, in narrow microchannels where the acoustic boundary layer thickness δ_{ve} is comparable to the channel depth D but much smaller than the channel width W and acoustic wavelength λ_0 ($\delta_{ve} \sim D \ll W \sim \lambda_0$), Vargas *et al.* (2022) reported a continuous increase in pressure with relaxation time, with pressure being proportional to $De^{1/2}$. However, this relationship does not hold for commonly used microchannels in acoustofluidics, where δ_{ve} is smaller and both D and W are comparable to λ_0 ($\delta_{ve} < D \sim W \sim \lambda_0$). Thus our findings highlight a remarkable differences in the behaviour of pressure waves in commonly used microchannels as compared with narrow microchannels, highlighting the unique attributes of the present study.

Generally, a fluid undergoes relaxation when exposed to external perturbations, and it depends on the relaxation time scale τ . In a viscous fluid, $\tau \sim 0$, and in an elastic body, $\tau \sim \infty$. Viscoelastic fluids have a relaxation time between the two extremes (Bird, Armstrong & Hassager 1977; Joseph 2013), and De represents the fluid relaxation time (τ) with respect to the time period of acoustic perturbation ($t_f = 1/\omega$). For viscoelastic fluids with $De \ll 1$ ($\tau \ll t_f$), stress generated by the perturbation relaxes faster than the actuation period, causing a low pressure amplitude. At high De ($\tau \gg t_f$), stress generated by the perturbation relaxes very slowly, showing higher incoming pressure amplitude compared with a Newtonian fluid ($De = 0$). Therefore, viscoelastic fluids exhibit a distinct behaviour

compared with Newtonian fluids due to the variations in fluid's elasticity, δ_{ve}^* and λ_{ve}^* , as shown in figure 4(a–d).

We introduce a parameter $\alpha = \lambda_{ve}^*/\delta_{ve}^* = \lambda_{ve}/\delta_{ve}$, shown in figure 4(e), to study the relative variation of the length scales related to the viscous shear wave. The viscous shear wave parameter α attains a value of approximately 2π for low elasticity ($De \ll 1$) and high elasticity fluids De ($De \gg 1$). For moderate elasticity fluids (moderate De values), α decreases up to $De \approx 10$, beyond which it increases. This trend can be attributed to the variations in δ_{ve}^* and λ_{ve}^* , providing deeper insights into the viscoelasticity of fluids. The variations in the incoming fields directly indicate changes in the AED of the fluid. We characterize AED using the dimensionless AED (E_{ac}^*), defined as the ratio of E_{ac} for a viscoelastic fluid to that of the base Newtonian fluid, $E_{ac}^* = E_{ac}^{ve}/E_{ac}^{bf}$, as shown in figure 4(e). Interestingly, at a fixed value of μ^* , we observe that, with increasing elasticity or De (keeping t_f fixed), E_{ac}^* increases, mirroring the variation in amplitude of the incoming pressure wave, as shown in figure 4(a). The rate of increase, however, varies across the different ranges of De . For low elasticity fluids ($De \ll 1$), the change in E_{ac}^* is negligible. Conversely, moderate elasticity fluids (moderate De) show a significant rise in E_{ac}^* with De , corresponding to a marked increase in incoming pressure wave amplitude in figure 4(a). Further increase in De results in a negligible change in the incoming pressure field, leading to a nearly fixed value of E_{ac}^* in highly elastic fluids ($De \gg 1$). Viscous effects dominate in low elasticity fluids, while elasticity effects surpass viscous effects in high elasticity fluids. Higher viscous effects indicate an energy dissipation state, whereas higher elasticity effects indicates an energy storage state. Thus, with increasing De , a viscoelastic fluid transitions from an energy dissipation state (relaxation mode or relaxing state of AED) to an energy storage state (frozen mode or freezing state of AED) where energy dissipation is minimized (Bird *et al.* 1977; Joseph 2013).

In the next section, we investigate the transition of AED with De at different μ_p^* and μ_s^* , that affects the ARF and particle migration. Our study unveils novel insights into the energy states of viscoelastic fluids under varying conditions, contributing significantly to the understanding of fluid behaviour in microfluidic environments exposed to the acoustic waves.

5.2. Effect of viscoelastic properties on acoustic energy density

Acoustic waves can transport energy without a net fluid transfer (Lighthill 1978). Viscous attenuation alters the acoustic field and AED in viscous fluids (Allegra & Hawley 1972). However, the impact of viscoelastic properties on AED in micro-confinements is not well studied. Therefore, we numerically analyse AED transition in a microchannel due to variations in the viscoelastic parameters μ_p^* , μ_s^* and De (see §§ 2.1 and 3). Using the theoretical formulations in § 2.2 for δ_{ve} , λ_{ve} and $\alpha (= \lambda_{ve}/\delta_{ve})$, we relate variations in dimensionless AED ($E_{ac}^* = E_{ac}^{ve}/E_{ac}^{bf}$) to the characteristics of viscous shear waves.

We depict the variation of E_{ac}^* with μ_p^* in figure 5(a) for three different cases: (i) small De ($De \leq 1$, low elasticity fluids), (ii) intermediate De ($1 < De \leq 100$, moderate elasticity fluids) and (iii) high De ($De > 100$, high elasticity fluids), with $\mu_s^* = 1$, $\rho^* = 1$ and $c^* = 1$ fixed in all cases. For low elasticity fluids ($De \leq 1$), viscous effects dominate, with $\delta_{ve}^* < \lambda_{ve}^*$ and $\alpha > 1$. The variation of δ_{ve}^* and λ_{ve}^* with μ_p^* is shown in figure 5(b–i) using solid and dashed lines, respectively. The corresponding variations in α are illustrated in figures 5(c) and 5(d). According to (5.1a–c) and figure 5(b–i), increasing μ_p^* amplifies δ_{ve}^* and viscous dissipation, reducing incoming fields and consequently the AED, as shown in figure 5(a–i). The decay is more rapid at smaller μ_p^* and slower at higher μ_p^* , due to a higher

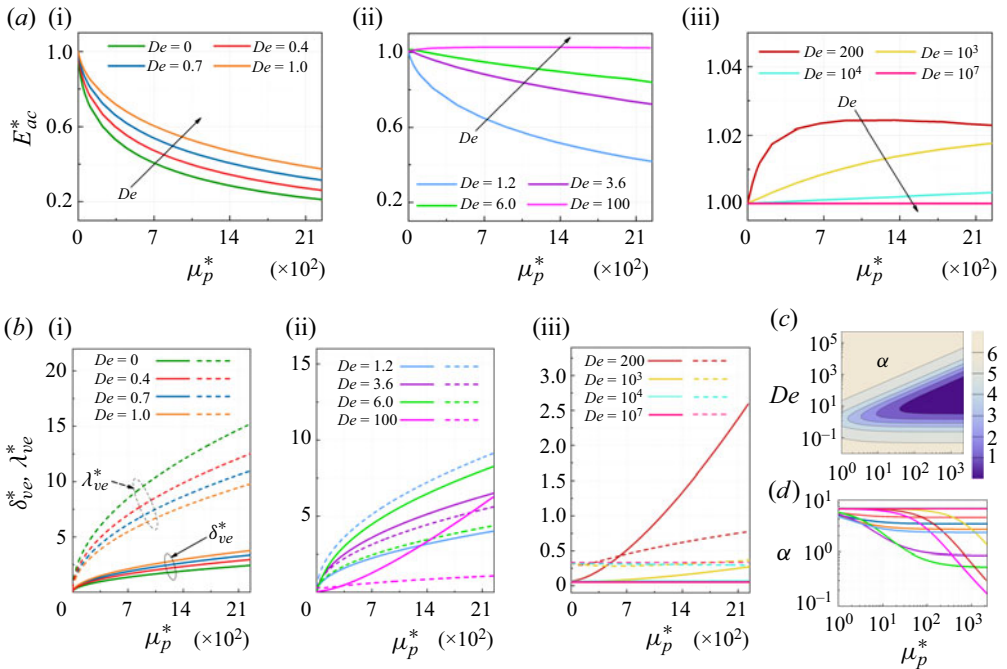


Figure 5. (a) Numerical variation of dimensionless acoustic energy density (E_{ac}^*) and corresponding (b) theoretical variation of δ_{ve}^* and λ_{ve}^* with μ_p^* at different De : (i) $De \leq 1$, (ii) $1 < De \leq 100$, (iii) $De > 100$. (c) Contour plot of α with De and μ_p^* . (d) Variation of α with μ_p^* at different De . Here, we consider $\mu_s^* = 1$, $\rho^* = 1$ and $c^* = 1$.

rate of change in δ_{ve}^* and α at smaller μ_p^* , which stabilizes at a higher μ_p^* (see figures 5a-i, 5b-i and 5c,d). Thus, viscoelastic fluids with $De \ll 1$ and $\tau \ll t_f$ exhibit energy dissipation at a faster rate similar to viscous fluids, depicting the relaxation mode. Interestingly, E_{ac}^* increases with De for all μ_p^* , because an increase in τ decreases α , leading to an increase in the incoming fields and energy storage, as mentioned in § 5.1. For moderate elasticity fluids ($1 < De \leq 100$), elastic effects start to dominate over viscous effects, with $\delta_{ve}^* > \lambda_{ve}^*$ and $\alpha < 1$ for $De > 3$ (see figures 5b-ii and 5c,d). In this range, E_{ac}^* decreases with μ_p^* , but the rate of decrease slows down due to enhanced elastic effects, indicating a reduced contribution of polymer viscosity to viscous dissipation (see (5.2a-c)). As De increases, the incoming pressure p_{in}^* rises (figure 4a), and E_{ac}^* approaches 1 for $De = 100$, suggesting a transition to a freezing state of AED (frozen mode) at all μ_p^* .

For high elasticity fluids ($De > 100$), elastic effects dominate over viscous effects, with $\delta_{ve}^* > \lambda_{ve}^*$ and $\alpha > 1$ (see figures 5b-iii and 5c,d). Here, E_{ac}^* becomes nearly independent of μ_p^* and De (see (5.3a-c)), as shown in figure 5(a-iii). Viscoelastic fluids with $De \gg 1$ and $\tau \gg t_f$ indicate energy storage, representing a freezing state of energy or frozen mode (Bird *et al.* 1977; Joseph 2013). The frozen mode shows a state of viscoelastic fluid where the AED is independent of De and μ_p^* . From figure 5(a-i-a-iii), we conclude that viscoelastic fluids exposed to ultrasound transition from a relaxing to a freezing state with increasing De , regardless of μ_p^* . This suggests that viscoelastic fluids have a higher AED compared with a Newtonian fluid for a fixed total viscosity. The increase in p_{in}^* with De in figure 4 supports this finding. At lower De , the effects of μ_p^* (see (5.1a-c)) is predominant, while at higher De , acoustic energy dissipation is determined by μ_s^* (see (5.3a-c)).

Fluid viscoelasticity affects ultrasound force field

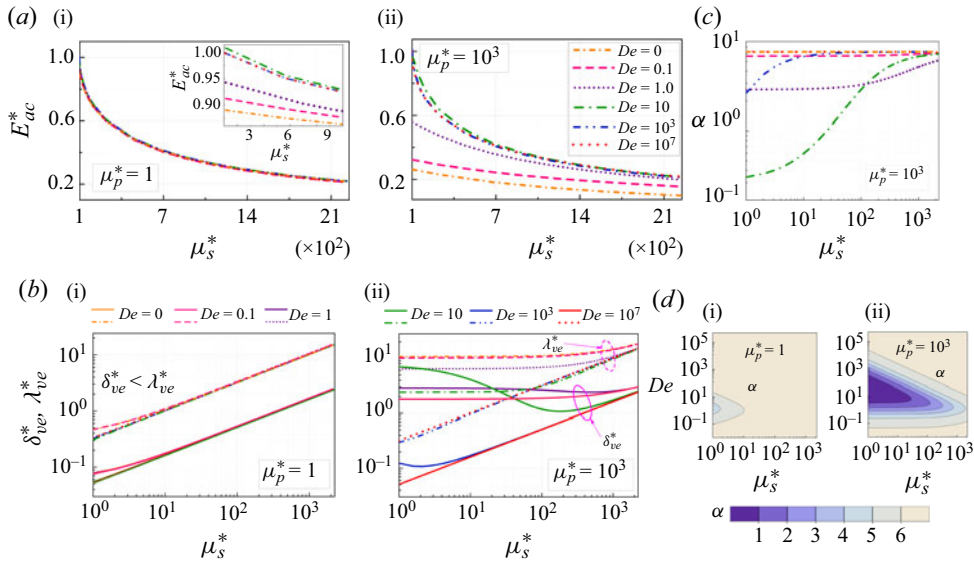


Figure 6. (a) Numerical variation of dimensionless AED (E_{ac}^*) and corresponding (b) theoretical variation of δ_{ve}^* and λ_{ve}^* with μ_s^* at different De (0, 0.1, 1, 10, 10^3 , 10^7) for (i) $\mu_p^* = 1$ and (ii) $\mu_p^* = 10^3$. (c) Variation of α with μ_p^* at different De . (d) Contour variation of α with μ_s^* and De for (i) $\mu_p^* = 1$ and (ii) $\mu_p^* = 10^3$. We consider $\rho^* = 1$ and $c^* = 1$.

To study the influence of solvent viscosity on AED of low, moderate and high elasticity fluids, the variation of E_{ac}^* with μ_s^* at different De and μ_p^* is presented in figure 6(a). For $\mu_p^* = 1$, figure 6(a-i) shows a decrease in E_{ac}^* with μ_s^* , which is due to the fact that an increase in μ_s^* leads to the growth of δ_{ve}^* , causing enhanced viscous dissipation and a decrease in p_{in}^* . Interestingly, for $\mu_p^* = 1$, E_{ac}^* appears to be independent of De at high μ_s^* , where variation of α with De is negligible (see figures 6b-i and 6d-i). The inset in figure 6(a-i) shows E_{ac}^* increases with De for low μ_s^* , accompanied by a small variation in α (see figure 6d-i). The variation of E_{ac}^* with μ_s^* and De for $\mu_p^* = 10^3$ is presented in figure 6(a-ii), showing a decrease in E_{ac}^* with μ_s^* similar to $\mu_p^* = 1$. Notably, E_{ac}^* varies significantly with De at smaller μ_s^* , attributed to the variation of δ_{ve}^* and λ_{ve}^* (see figure 6b-ii) and the change in α from < 1 to 2π (see figure 6c). At higher μ_s^* , AED follows the same trend as that at lower μ_s^* with increasing De , but due to a higher viscous dissipation, the freezing state E_{ac}^* reduces to a smaller value. In summary, viscoelastic fluids transits from a relaxing to a freezing state in AED for all μ_s^* . In the freezing state, E_{ac}^* decreases with increasing μ_s^* , with the rate of decrease dependent on μ_p^* and De . Interestingly, increasing μ_p^* (or μ^*) does not always result in a decrease in the pressure amplitude – at higher De , μ_p^* has negligible effect on pressure field and AED. This contrasts with the study by Vargas *et al.* (2022) that reported a continuous decrease in pressure wave amplitude with viscosity varying as $\mu^{-3/5}$ in narrow microchannels. The difference likely arises because they considered δ_{ve}^* only as a function of viscosity and neglected higher-order viscous effects by assuming $2D/\lambda_0 \ll 1$, which is applicable to narrow channels. In our study, $D \sim \lambda_0$ and therefore we consider the effects of both viscosity and elasticity in δ_{ve} and λ_{ve} (see (2.20) and (2.21)).

In the following section, we discuss how variations in the acoustic energy transition affect the ARF on a particle in a viscoelastic fluid.

5.3. Effect of acoustic energy transitions on acoustic radiation force

The ARF can induce particle migration in a fluid exposed to ultrasound (Barnkob *et al.* 2010; Bruus 2012*b*). The effects of boundary layer formation over particles suspended in unbounded fluids of different viscoelastic properties on the ARF are discussed in Doinikov *et al.* (2021*b*). However, most acoustomicrofluidic devices consider microchannels of dimensions of the order of the acoustic wavelength. Here, apart from boundary layer formation over the particles, the boundary layer formation on the channel walls and dissipation in viscoelastic fluid also become significant, influencing ARF and particle migration, which is missing in the literature. We focus on the dynamics of particle migration in microchannels and for $a \ll \lambda_0$. We consider the influence of viscoelastic fluid properties on ARF, characterized by AED (§ 5.2) and ACF. In contrast to Doinikov *et al.* (2021*a,b*), we successfully decouple the effects of E_{ac}^{ve} and Φ on ARF theoretically, as described in (2.34) in § 2.3. Our approach considers the ABL formation on both the microchannel walls and the particles, reflected in AED and ACF, respectively. From (2.34), we find that ARF is directly proportional to AED and ACF. Therefore, the ABL formation on the channel walls and the consequent variation in AED with μ_p^* , μ_p^* and De (given in § 5.2) significantly impacts ARF and particle migration. Further, we observe that increasing the fluid elasticity enhances the AED and consequently the ARF due to boundary layer formation over the channel walls. However, we do not observe any change in the sign of the force as compared with Doinikov *et al.* (2021*b*), even with the influence of the channel boundary layers, likely due to the high driving frequency used in our system (order of MHz).

To further differentiate the effect of viscoelasticity on AED from that on ACF, we analyse the relative variation in ACF for a particle in fluids with and without viscoelasticity, as detailed in supplemental material § 4.1. This variation is expressed as $\Omega = \{\Phi(\kappa_p^*, \rho_p^*, \delta_{ve}^*, \lambda_{ve}^*) - \Phi(\kappa_p^*, \rho_p^*, 0, 0)\} / \Phi(\kappa_p^*, \rho_p^*, 0, 0)$ in percentages. We find that the values of Ω vary by up to 0.3%, 3.75%, 2.6%, 11.8%, 27% and 39% for polystyrene (PS), MESC2.10 cells, melamine resin, polymethacrylate, silica and Pyrex particles, respectively, in viscoelastic fluid with $\mu_s^* = 1$, $\mu_p^* = 10$, $De = 200$, $\rho^* = 1.005$ and $c^* = 1$. To study the effect of viscoelastic parameters and AED transition on particle migration dynamics inside a microchannel, we focused on PS microparticles for which the ACF in a viscoelastic fluid, compared with that in the base Newtonian fluid, is minimal (only 0.3%), as given in supplemental material § 4.1. Therefore, the dimensionless acoustic radiation force F_{rad}^* ($F_{rad}^* = F_{rad}^{ve} / F_{rad}^{bf}$) follows the same trend as the variation of E_{ac}^* with the viscoelastic properties of the fluid, as detailed in supplemental material § 4.2.

5.4. Effect of viscoelastic properties on particle migration

A particle suspended in a fluid with a positive ACF experiences ARF towards acoustic pressure node (Barnkob *et al.* 2010; Bruus 2012*b*). Here, through appropriate channel design and actuation, a pressure node is formed at the channel centre, as shown in figure 4(*a*). We investigate how changes in the AED and acoustic force field, resulting from the viscoelastic parameters μ_p^* , μ_s^* and De , affect the particle migration dynamics. For the first time, we conduct experiments to study particle migration dynamics in a viscoelastic fluids within a microchannel exposed to ultrasound and validate the theoretical expressions given by (2.40) and (2.42) in § 2.4. We use PS beads suspended in PEO and PVP-based viscoelastic fluids, offering a positive ACF as obtained from (2.35).

Fluid viscoelasticity affects ultrasound force field

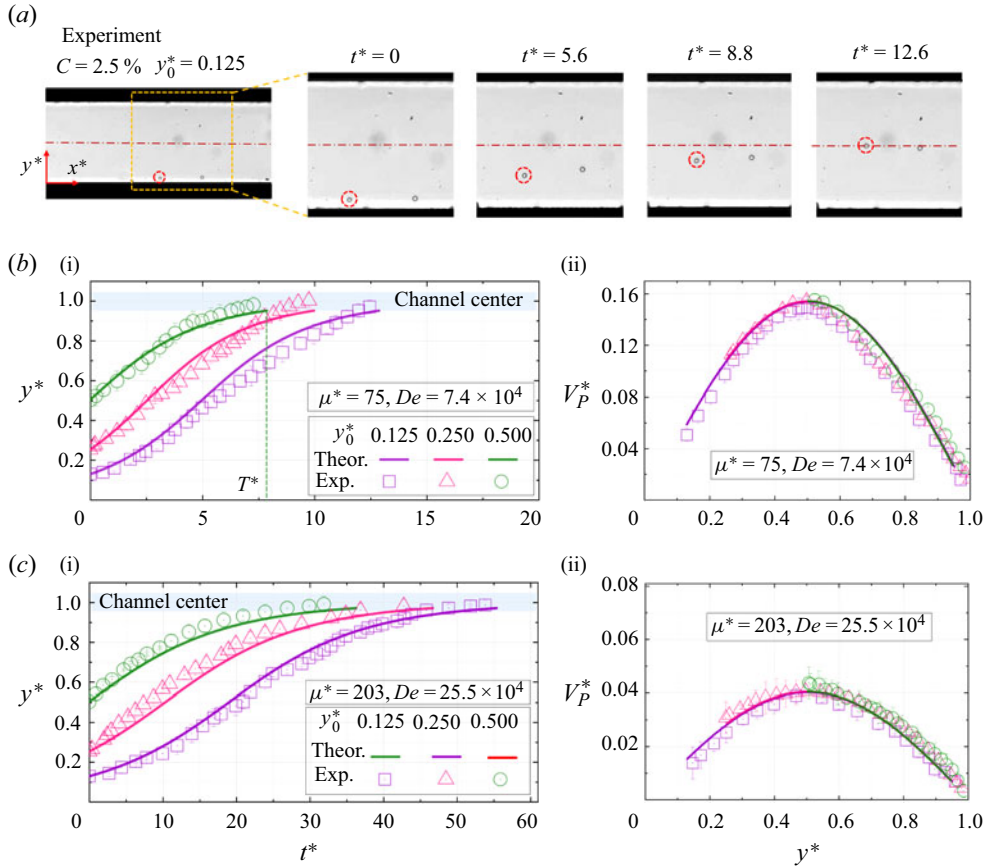


Figure 7. (a) Experimental images showing the time history of the transverse position of a particle released from $y_0^* = 0.125$ in a PEO 0.4 MDa solution with $C = 2.5\%$. The particle is marked by a red dashed circle. Comparison of theoretical and experimental variation of (i) dimensionless particle trajectory (transverse location vs time of migration) and (ii) dimensionless particle velocity along y^* in PEO 0.4 MDa at two polymer concentrations: (b) $C = 2.5\%$: $\mu^* = 75$ ($\mu_s^* = 1, \mu_p^* = 74$), $De = 7.4 \times 10^4$ and (c) $C = 3.5\%$: $\mu^* = 203$ ($\mu_s^* = 1, \mu_p^* = 202$), $De = 25.5 \times 10^4$. The particle is released from initial locations $y_0^* = 0.125, 0.25$ and 0.5 . The dimensionless central migration time is represented as T^* .

We present the trajectories and velocities of PS particles during their migration, with different initial locations ($y_0^* = y_0/(W/2)$), $y_0^* = 0.125, 0.25$ and 0.50 , in PEO 0.4 MDa solutions at two different concentrations, $C = 2.5\%$ and 3.5% , in figure 7. For PEO 0.4 MDa solution with $C = 2.5\%$, the fluid properties are: $\mu^* = 75$ ($\mu_s^* = 1, \mu_p^* = 74$), $De = 7.4 \times 10^4$, $\rho^* = 1.025$, $c^* = 1.011$, $\xi \approx 1$. Similarly, the properties for $C = 3.5\%$ are: $\mu^* = 203$ ($\mu_s^* = 1, \mu_p^* = 202$), $De = 25.5 \times 10^4$, $\rho^* = 1.045$, $c^* = 1.015$, $\xi \approx 1$ (Zimm 1956; Ebagninin, Benchabane & Bekkour 2009; Faroughi *et al.* 2020). We normalize the instantaneous locations of the particles with the half-width of the channel, $y^* = y/(W/2)$. We define an acoustic time scale ($t_{ac} = D\lambda_0\mu/a^2E_{ac}\Phi$) based on the solvent (DI water) to non-dimensionalize the migration time as $t^* = t/t_{ac}$. The local velocity of the particles is normalized using a reference velocity ($V_{ref} = (W/2)/t_{ac}$), the dimensionless particle velocity $V_P^* = V_P/V_{ref}$. The particle diameter is $15 \mu\text{m}$ and

therefore blockage ratio becomes $\beta = a/(W/2) = 0.0375$. The transducer is operated at a driving voltage $U_{pp} = 13.2$ V, where $U_{pp}^* = U_{pp}/U_{pp}^{min} = 1.14$.

We initially study the effect of varying ARF across the channel width (S-BAW or y -direction) on particle migration in a viscoelastic fluid. Since the ARF acts only along the y direction, particle translation is one-dimensional in the x - y plane, with negligible drift in the x direction. The time-lapsed experimental images showing migration of a 15 μm PS particle with $y_0^* = 0.125$ in PEO 0.4 MDa solution of $C = 2.5\%$ is shown in figure 7(a). The corresponding time evolution of particle position (y^*) and particle migration velocity (V_p^*) are shown in figures 7(b-i) and 7(b-ii), respectively. Under an acoustic field, the particles migrate from their initial positions to a final equilibrium position with a varying velocity, and the final equilibrium position is represented by $y^* = 1 \pm 0.05$ (the central pressure nodal region is indicated as a band in figure 7a). The value of V_p^* shows a non-monotonic variation during its migration, where V_p^* is found to be small closer to the channel centre and wall, but becomes maximum closed to $y^* \approx 0.5$, shown in figure 7(b-ii). We compare the experimental data with the predictions from the theoretical expressions given by (2.40) and (2.42) in § 2.4, which shows a close agreement, with $V_p \propto \sin(2k_y y)$. The maximum velocity seen at $y^* \approx 0.5$ is due to the higher acoustic radiation force, which becomes zero at the walls and the channel centre, here, $F_{rad} \propto E_{ac}^{ve} \sin(2k_y y)$, as given by (2.40).

To further investigate the effect of initial locations of a particle on acoustic migration characteristics in viscoelastic fluids, we consider particles at $y_0^* = 0.125, 0.25$ and 0.5 . For PEO fluid with $C = 2.5\%$, $\mu^* = 75$ and $De = 7.4 \times 10^4$, the particle trajectories change with the initial location and the migration time to reach the centre of the channel decreases with increase in the y_0^* , illustrated in figure 7(b-i). It is interesting to observe that the migration velocities across y^* are found to follow a fixed curve, irrespective of the values of y_0^* , illustrated in figure 7(b-ii), agreeing with our theoretical prediction (2.42).

Viscoelastic fluids show a coupled variation of viscous and elastic properties with increasing polymer concentration (Ebagninin *et al.* 2009; Joseph 2013). We study the coupled variation of μ^* (or μ_p^* , where $\mu_s^* = 1$) and De on acoustic particle migration in figures 7(b-i,ii) and 7(c-i,ii). At a fixed y_0^* , a coupled increase in both μ^* and De slows down particle migration due to the combined increase in drag force and decrease in acoustic energy density, shown in figure 7(c-i,ii). The value of V_p^* is found to be smaller at a higher μ^* and De . However, the effect of initial location remains same as figure 7(b-ii). A quantitative comparison between theoretical predictions and experimental data shows a close agreement in terms of the particle trajectory and velocity variations within 10%.

Now we discuss the individual effects of μ^* and De and the corresponding AED transition on acoustic particle migration, theoretically and experimentally, as shown in figure 8. We consider PVP 0.36 MDa ($C = 0.1\%$, $\mu^* = 1.9$, $\mu_s^* = 1$, $\mu_p^* = 0.9$, $De = 91$), PEO 0.4 MDa ($C = 0.2\%$, $\mu^* = 1.9$, $\mu_s^* = 1$, $\mu_p^* = 0.9$, $De = 178$) and Newtonian fluid (DI water +0.3% Glycerol, $\mu^* = 1.9$, $De = 0$) all having a fixed ρ^* ($\rho^* \approx 1.007$) and c^* ($c^* \approx 1.003$), keeping μ^* fixed and only varying De , as shown in figure 8. Here, we find that an increase in the elasticity or De of the fluid enhances the particle migration, shown by a reduced central migration time ($T^* = t^*|_{y^* \approx 1}$) and a higher V_p^* in figures 8(a) and 8(b), respectively. Therefore, as compared with the Newtonian fluid ($De = 0$), particles migrate faster in PEO 0.4MDa fluid with $De = 178$. This is mainly because of the acoustic energy transition with De , as discussed in § 5.2. Due to the viscous nature, the Newtonian fluid exhibits higher viscous dissipation and remains in the relaxation mode, giving rise to a low AED in the fluid. However, in high elasticity fluids, the elastic nature helps to reduce the viscous dissipation and store the energy, offering

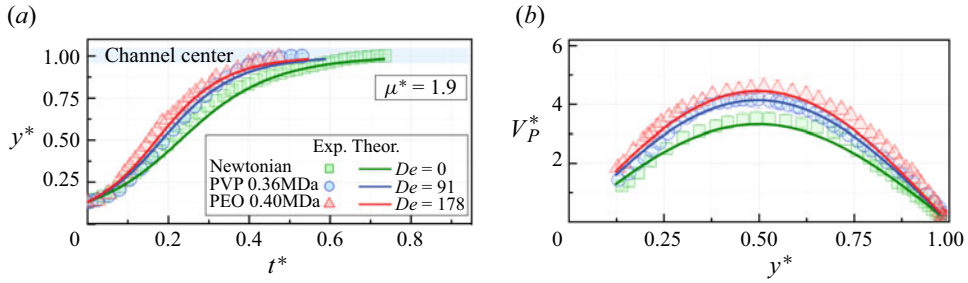


Figure 8. Comparison of theoretical and experimental variation of dimensionless (a) trajectory (y^* vs t^*) and (b) velocity (V_p^* vs y^*) of particle in PEO 0.4 MDa, PVP 0.36 MDa and Newtonian (DI water+0.3% glycerol) fluid of constant viscosity $\mu^* = 1.9$. The initial location of particle is considered as $y_0^* = 0.125$. Each data point corresponds to a value averaged over repeated experiments.

high AED and consequently higher ARF. Here, we observe a strong agreement between our experimental data and the predictions from our theory and simulations, all of which suggest that the AED transition is attributed to the fluid elasticity giving rise to a faster particle migration in viscoelastic fluids than in Newtonian fluid.

Next, we discuss the effect of fluid elasticity and the corresponding AED transition on the particle migration dynamics at different μ_p^* and μ_s^* , presented in figure 9. We express the theoretical variation of particle migration time in terms of dimensionless central migration time T^* , which is defined as the ratio of the time taken by a particle to reach the channel centre (nodal plane) ($t_c = t|_{y^* \approx 1}$) to the acoustic time scale (t_{ac}), $T^* = t_c/t_{ac}$. We illustrate the variation of T^* with μ_p^* in figure 9(a) for three different scenarios: (a) low elasticity fluids ($De \leq 1$), (b) moderate elasticity fluids ($1 < De \leq 100$) and (c) high elasticity fluids ($De \geq 200$), with $\mu_s^* = 1$, $\rho^* = 1$ and $c^* = 1$.

For low elasticity fluids ($De \leq 1$), viscous effects dominate and fluids are in the relaxation state. Therefore, an increase in μ_p^* amplifies the viscous dissipation, and consequently the AED and ARF decrease, as shown in figure 5(a-i). Moreover, with increase in μ_p^* drag forces increases. The combined effects of these variations gives rise to a significant increase in T^* with μ_p^* in figure 9(a-i). However, an increase in De leads to an increase in the AED in the fluid, which causes a decrease in the T^* as well as the rate of increase in T^* with μ_p^* . The influence of De on T^* becomes more pronounced at a higher μ_p^* . For moderate elasticity fluids ($1 < De \leq 100$), T^* increases with μ_p^* at a moderate rate in figure 9(a-ii). Here, the elastic effects start dominating viscous effects, fluid starts to transition from the relaxation mode to the frozen mode, as shown in figures 4(e), 5(a-ii) and 5(b-ii). The increased E_{ac}^* in moderate elasticity fluids compared with low elasticity fluids causes a higher ARF, which reduces T^* as well as rate of increase in T^* with μ_p^* in figure 9(a-ii). A further increase in De leads to an increase in AED, causing a further decrease in T^* as well as the rate of increase in T^* with μ_p^* , as illustrated in figure 9(a-ii). For high elasticity fluids ($De > 100$), T^* slowly increases with μ_p^* and is nearly independent of De , as shown in figure 9(a-iii). Here, elastic effects suppress viscous effects, and fluid attains the frozen state, as shown in figures 4(e), 5(a-iii) and 5(b-iii). Therefore, E_{ac}^* and thus the ARF attain their maximum values and becomes independent of De and μ_p^* . This phenomenon reduces T^* and rate of increase in T^* with μ_p^* in figure 9(a-iii). In summary, the higher elasticity fluids show shorter central migration time as compared with low elasticity fluids in all range of μ_p^* due to transition of AED from a relaxation mode to a frozen mode.

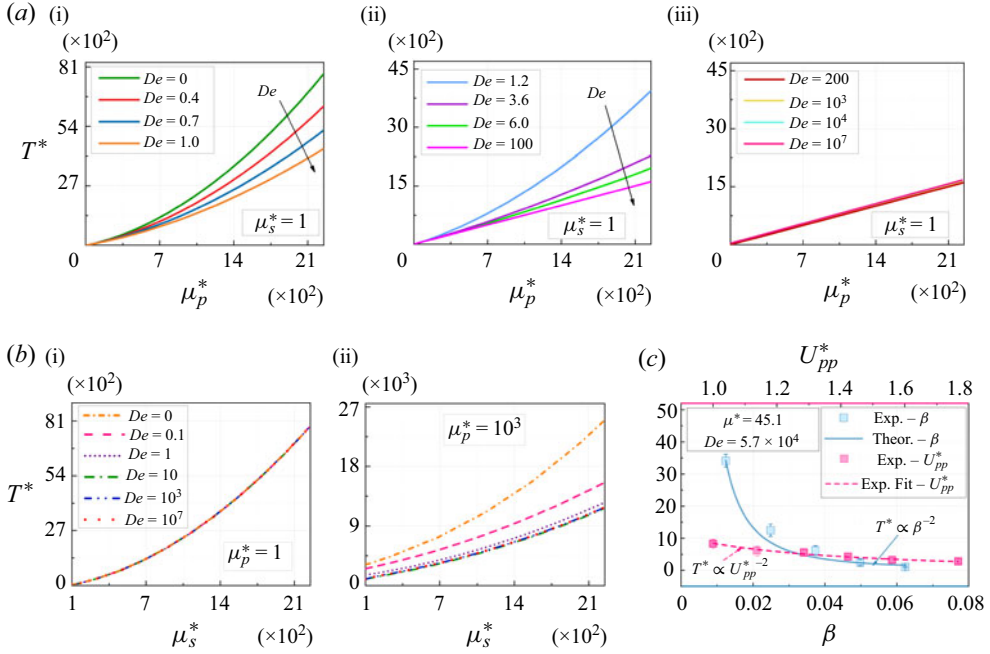


Figure 9. Theoretical variation of (a) dimensionless particle central migration time (T^*) with μ_p^* at different De : (i) $De \leq 1$, (ii) $1 < De \leq 100$, (iii) $De > 100$ for $\mu_s^* = 1$, and (b) T^* with μ_s^* at different De for (i) $\mu_p^* = 1$ and (ii) $\mu_p^* = 10^3$. Here, $\beta = 0.0375$, $U_{pp}^* = 1.14$, $\rho_p^* = 1.05$ and $y_0^* = 0.125$. (c) Experimental variation of T^* with blockage ratio (β , at $U_{pp}^* = 1.14$) and dimensionless peak-to-peak voltage (U_{pp}^* , at $\beta = 0.0375$) for PEO 1 MDa solution with $C = 1.05\%$ ($\mu^* = 45.1$, $De = 5.7 \times 10^4$), where $y_0^* = 0.125$. The theoretical variation of T^* with β from (2.40) is shown by a solid line, where $T^* \propto \beta^{-2}$. For T^* with U_{pp}^* , the experimental fit becomes $T^* \propto U_{pp}^{*-2}$.

We depict the variation of T^* with μ_s^* at different De and μ_p^* in figures 9(b-i) and 9(b-ii). For $\mu_p^* = 1$, T^* consistently increases with μ_s^* and is independent of De , as shown in figure 9(b-i). This can be attributed to the viscous dissipation and consequent decrease in E_{ac}^* with μ_s^* (refer to figure 6a-i). For $\mu_p^* = 10^3$, T^* increases with μ_s^* but decreases with De for smaller De and becomes independent of De at higher De ($De = 10^3$ and 10^7), as illustrated in figure 9(b-ii). Here, the fluid response transition from the relaxation mode to the frozen mode, causing a decrease in T^* with increasing De for low elasticity and moderate elasticity fluids. However, in high elasticity fluids, the E_{ac}^* attains a maximum value and then becomes independent of De , as similar to figure 6(a). In summary, an augmentation in the solvent viscosity of a viscoelastic fluid decelerates particle migration and concurrently suppresses elastic effects, particularly at lower polymer viscosity range.

In the above analysis, we consider a fixed particle size or blockage ratio ($\beta = a/(W/2) = 0.0375$) and dimensionless driving voltage U_{pp}^* ($U_{pp}^* = U_{pp}/U_{pp}^{\min} = 1.14$), which indicate the acoustic power input. We perform theoretical and experimental investigations on the effects of β and U_{pp}^* on particle migration in a viscoelastic fluid in figure 9(c). Here, β is varied experimentally by varying the particle size between 5 and 25 μm . The variation of T^* with β and U_{pp}^* is depicted in figure 9(c) for PEO 1 MDa solution with $C = 1.05\%$, with $\mu^* = 45.1$, $\mu_p^* = 44.1$, $\mu_s^* = 1$, $De = 5.7 \times 10^4$, $\rho^* = 1.017$ and $c^* = 1.005$. We find that the central migration time decreases with an increase

in the blockage ratio or particle size. This decrease is primarily attributed to the rise in the ARF, evident from (2.42), where $T^* \propto \beta^{-2}$, similar to the Newtonian case (Barnkob *et al.* 2010). We find that particles migrate more rapidly towards the node at higher powers and lower μ^* owing to the increase in AED and ARF. A power-law fit to the experimental data shows $T^* \propto U_{pp}^{*-2}$, agreeing with the Newtonian case (Barnkob *et al.* 2010). The dependency of T^* with β and U_{pp}^* is also studied with two other PEO 1 MDa solutions: $C = 0.74\%$ with $\mu^* = 21.3$, $De = 3.7 \times 10^4$; and $C = 1.05\%$ with $\mu^* = 45.1$, $De = 5.7 \times 10^4$; $C = 1.4\%$ with $\mu^* = 69.5$, $De = 1.1 \times 10^5$. Here, the rate of change of T^* increases/decreases depending upon μ^* and De of the fluid, as presented in supplemental material § 4.3.

In summary, particle migration in viscoelastic fluids within a microchannel is significantly influenced by the fluid properties and acoustic boundary layer formation. From a biological standpoint, fluids such as blood, plasma, mucus, saliva, sputum, synovial fluid, protein solution and hydrogel have relaxation times ranging from 10^{-5} to 10^{-2} s (Thurston 1972; Rainer & Ribitsch 1985; Stokes & Davies 2007; Pan *et al.* 2009; Li *et al.* 2016; Chaudhuri *et al.* 2020), thus categorized as moderate and high elasticity fluids. Our study shows that changes in fluid elasticity or De causes the AED transition from the dissipation state to the storage state. This transition increases the ARF and accelerates particle migration. At a fixed input power, viscoelastic fluid in a microchannel acts as an energy dissipation device at low De (low elasticity) and as an energy storage device at higher De (high elasticity). Therefore, our study suggests that the Newtonian fluid assumption may not be valid for bio-fluids under all operating conditions. Moreover, by carefully controlling De , it is possible to manipulate the particle migration dynamics, at a fixed power. The outcome of the present study may be crucial for designing effective microfluidic systems for bio-fluids.

6. Conclusions

We investigated the behaviour of viscoelastic fluids exposed to ultrasound fields in a microchannel. We studied the effects of viscoelastic parameters and the formation of ABLs on the channel walls, on AED and consequently the particle migration dynamics. Our findings show that, with increasing fluid elasticity or Deborah number (De), viscoelastic fluids transition from an energy dissipation state (relaxation mode) to an energy storage state (frozen mode). For low elasticity fluids ($De \leq 1$), viscous effects dominate, leading to rapid energy dissipation. For moderate elastic fluids ($1 < De \leq 100$), elastic effects start to dominate, and the fluid begins to store acoustic energy. In high elasticity fluids ($De > 100$), elastic effects become predominant, leading to higher AED that are nearly independent of polymer viscosity and De . In low elasticity fluids, polymer viscosity significantly reduces the AED, but its effect diminishes with increasing elasticity. Solvent viscosity reduces the AED in all cases but is more dominant in high elasticity fluids. Thus, a viscoelastic fluid-filled microchannel acts as an energy dissipation device at low De and as an energy storage device at high De . By controlling the viscoelastic and acoustic parameters, fluid viscoelasticity can accelerate or decelerate a particle at a constant power input. Our experiments and theoretical analysis revealed that particle migration in viscoelastic fluids is faster than that in Newtonian fluids of comparable viscosity due to the AED transition from the relaxation to the frozen mode. In all elasticity regimes, the central migration time (T^*) increases with polymer and solvent viscosities but decreases with De . Higher solvent viscosity decelerates particle migration and suppresses elastic effects, especially at lower polymer viscosities. Considering these findings, and recognizing that bio-fluids

typically exhibit moderate to high elasticity, it becomes evident that assuming a Newtonian behaviour for such fluids may not always be valid in acoustofluidics. By adjusting the De , it will be possible to effectively control particle migration dynamics in microfluidic systems for bio-fluid applications.

Supplementary material. Supplementary material are available at <https://doi.org/10.1017/jfm.2024.965>.

Acknowledgements. The authors appreciate the support received from CNNP, IIT Madras for the device fabrication.

Funding. A.K.S. expresses gratitude to the Department of Science & Technology (DST), Government of India, for the financial support through the Swarnajayanti Fellowship Award under grant no. DST/SJF/ETA-03/2017-18; and acknowledges the support provided by the Ministry of Education, Government of India, under IoE Phase II project.

Declaration of interests. The authors report no conflict of interest.

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